

# Electrolyser innovations PEM, alkaline, SOEC, and AEM

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Hydrogen Tech World Conference, Essen  
26<sup>th</sup> June 2024

# Agenda

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1. Innovations in alkaline electrolysis
2. Innovations in PEM electrolysis
3. Innovations in PEM and alkaline electrolyser safety
4. Innovations in solid oxide electrolysis
5. Innovations in AEM electrolysis
6. Innovation or chaos?
7. Innovation in electrolyser manufacturing
8. Innovation in electrolyser supply chains

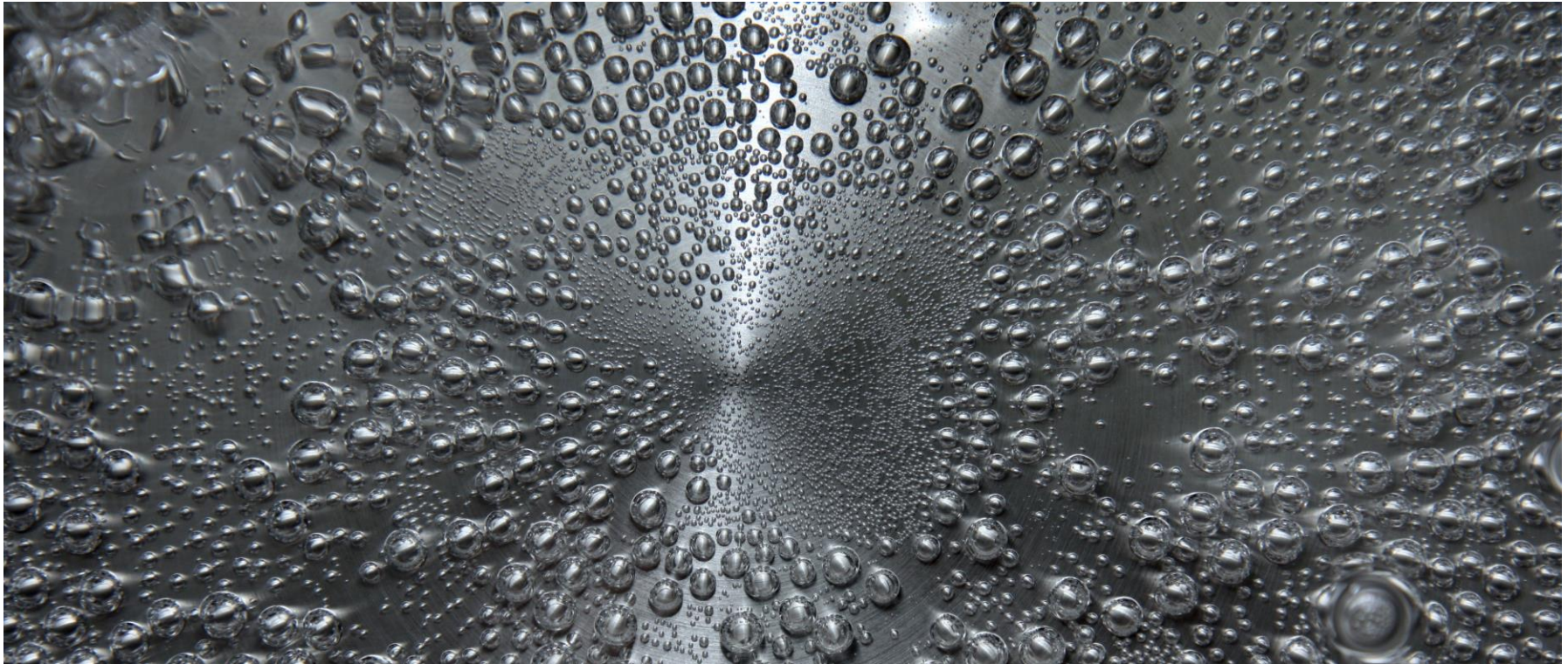
# Innovations in alkaline electrolysis

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A typical 400 kW PEM / AEM / Alkaline stack generates 120 kW of heat. Should an electrolyser produce heat, or hydrogen? Reducing resistance is a key path to improving efficiency and reducing the BOP costs of heat exchangers and cooling towers.



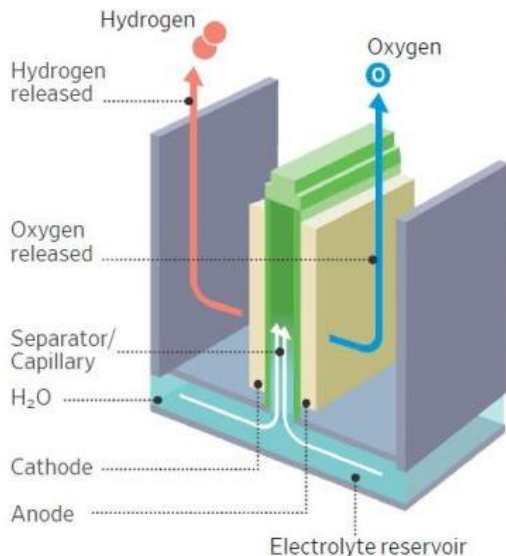
Hydrogen and oxygen gas bubbles on the electrolyser electrodes or membrane increase resistance and reduces efficiency. Hysata's bubble-free electrolysis addresses this issue.



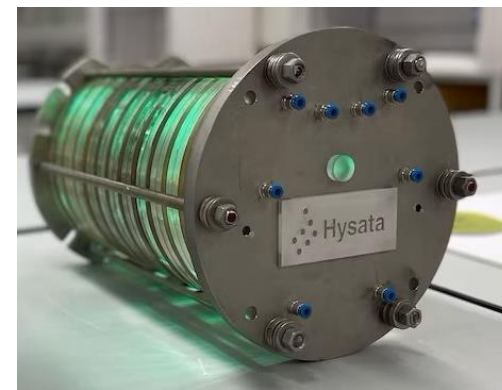
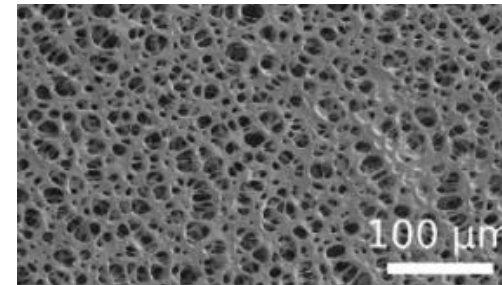


# Hysata proposed cell integration into low-cost stack. High efficiency reduces waste heat generation and reduces BOP cooling cost.

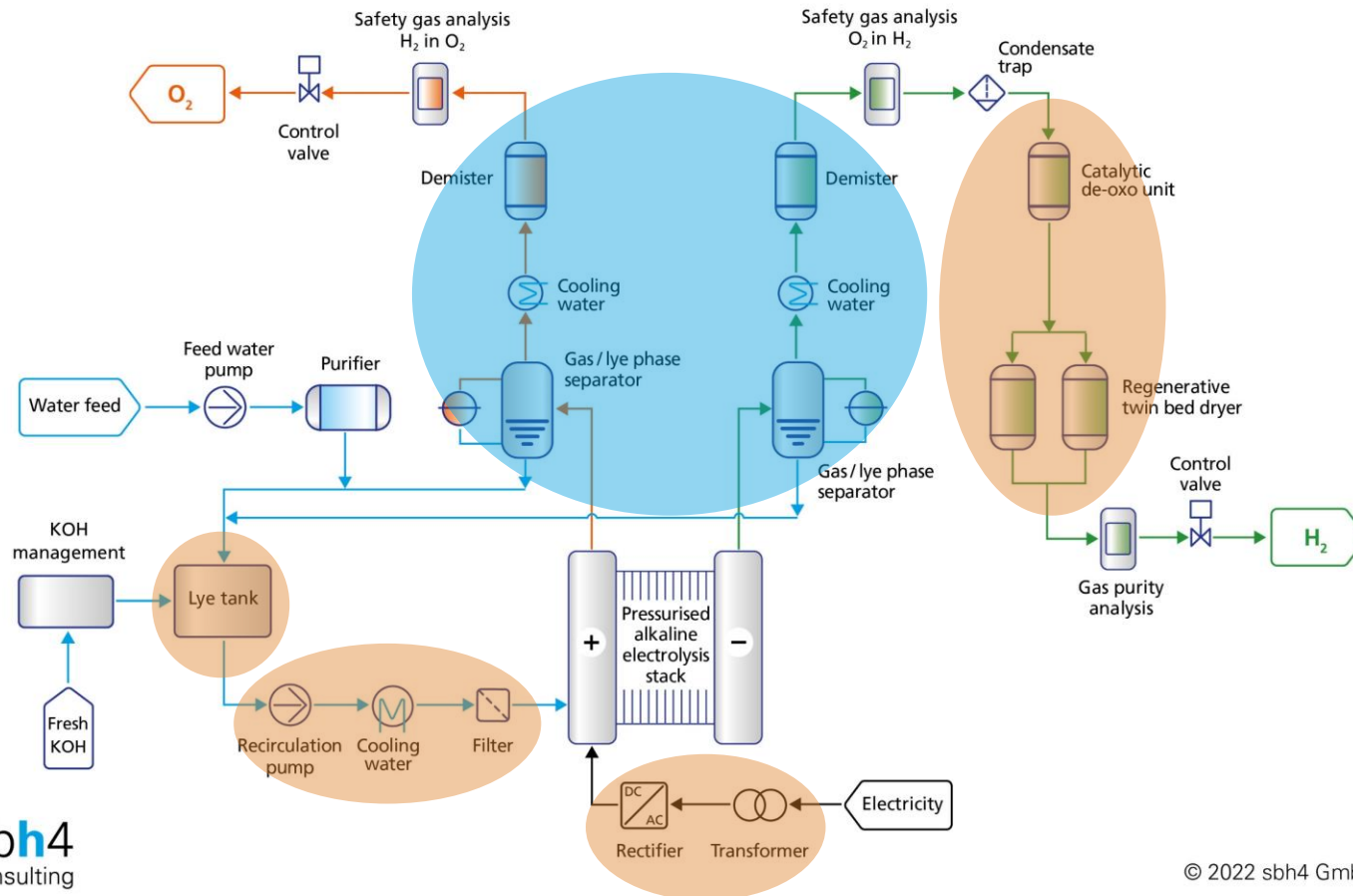
Rather than surrounding the electrodes, water is drawn up to the electrodes using capillary action. That means bubbles don't form on the anode and cathode and less energy is wasted, Hysata says.



- NiFeOOH Oxygen electrocatalyst
- Pt/C Hydrogen electrocatalyst
- 27 wt% KOH lye electrolyte
- 80 – 85 °C operating temperature
- 95% efficiency (HHV) at 0.8 A/cm<sup>2</sup> current density
- 100% efficiency (HHV) at 0.3 A/cm<sup>2</sup> current density
- 39.4 to 41.5 kWh / kg H<sub>2</sub>
- Porous, hydrophilic polyether sulphone (PES) capillary separator

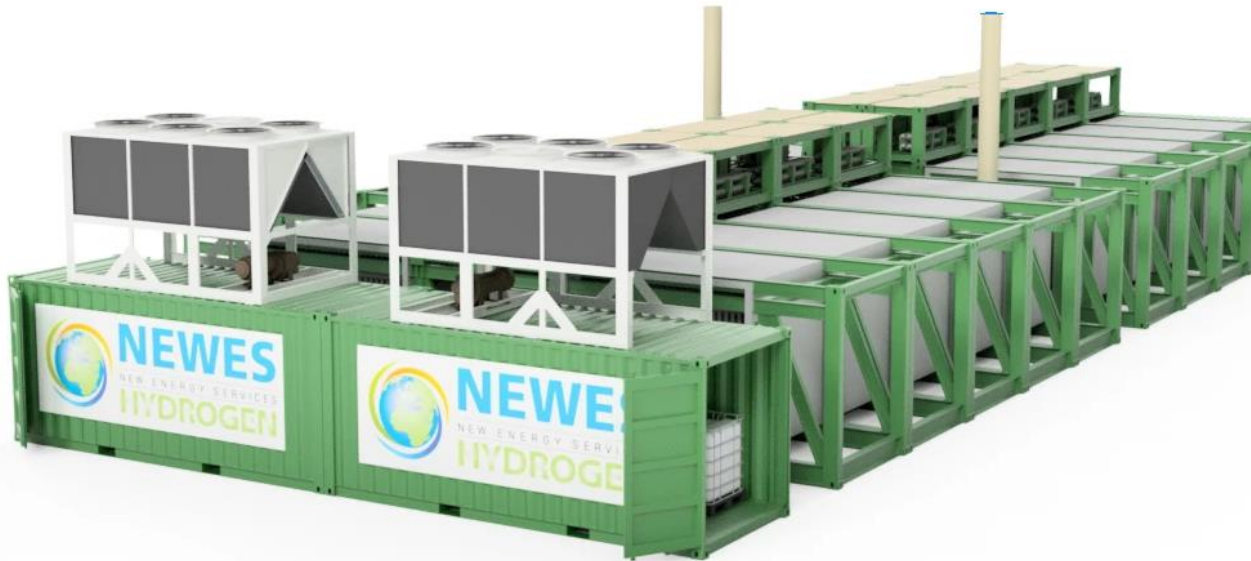


# Pressurised alkaline electrolysis process



Hysata high-efficiency, capillary-fed, zero bubble pressurised alkaline electrolysis results in BOP cost reductions compared to other pressurised alkaline electrolysis systems due to reduced size of power management, less cooling requirement and elimination of gas / liquid separation

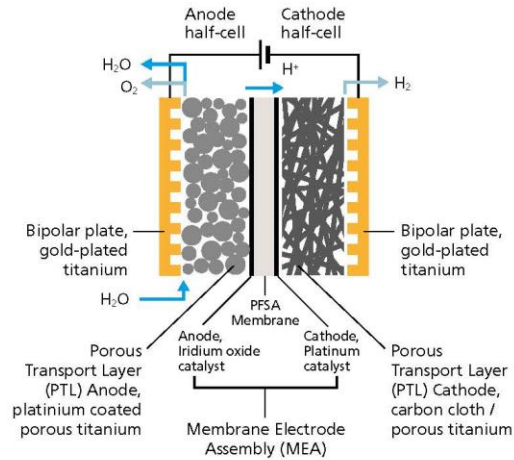
High pressure hydrogen for ammonia production or hydrogen mobility.  
Newes, NL. Tested 1.5 kW alkaline electrolyser with 140 bar hydrogen  
delivery at 99.3% purity in 2022, target to achieve 350 bar in 2023.



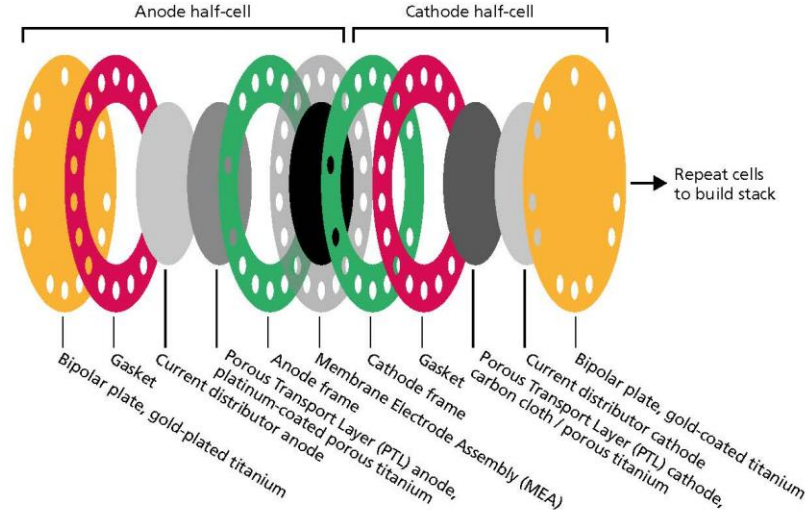


# Innovations in PEM electrolysis

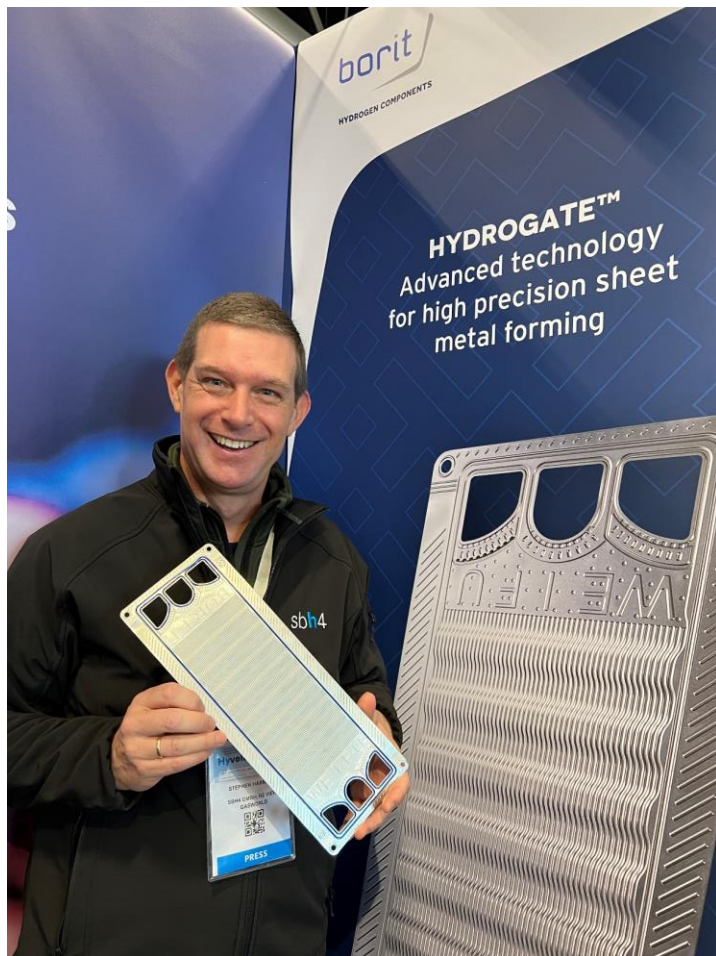
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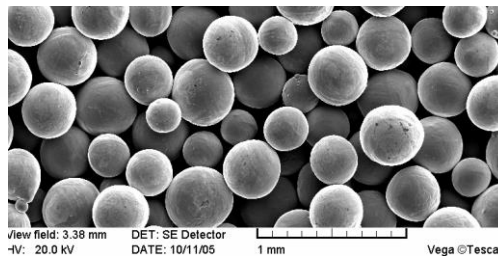
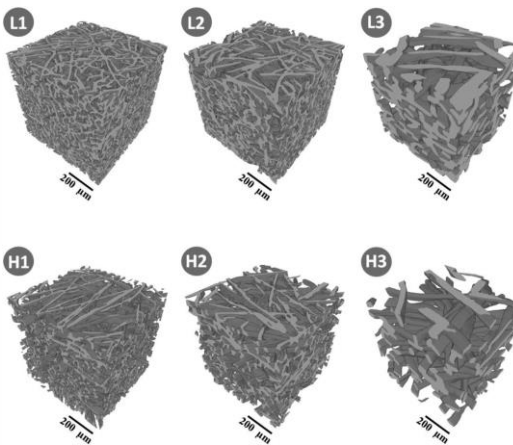
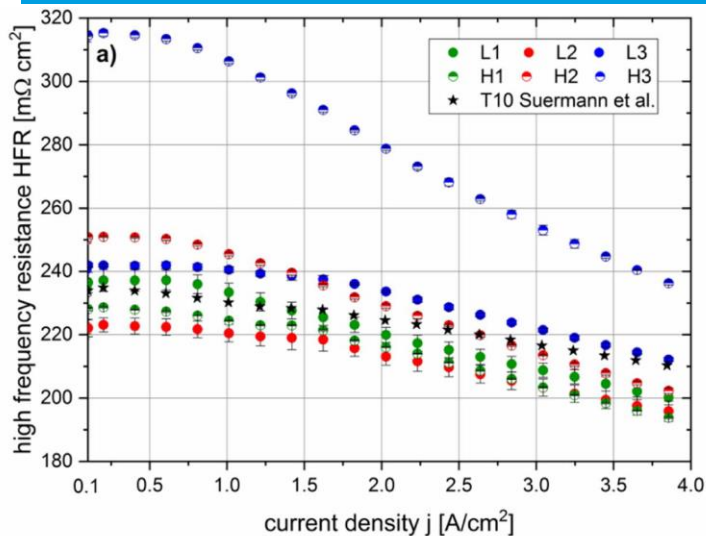
PEM – Proton Exchange Membrane or Polymer Electrolyte Membrane  
PTL – Porous Transport Layer  
MEA – Membrane Electrode Assembly  
BP or BPP – Bipolar Plate  
PFSA – Perfluorosulfonic acid ionomer, eg Nafion™



- Classical PEM stack architecture relies on precious metals: gold (BPP coating), iridium (anode) and platinum (cathode).
- Metallic components (BPP, PTL) are built around titanium – a metal in high demand for building nuclear submarines and apple phones!
- Manufacturing is complex due to processing of flexible membrane that is boiled, then coated with the catalytic powders.
- Assembly requires mechanical compression to retain gases at 20 to 30 bar.
- Gaskets and seals are critical to avoid internal and external leakages.



Sintered titanium powder mesh has historically been the standard PTL material, but sintered titanium fibres (eg Bekaert) are now established and can improve PTL and stack performance through reduced electrical resistance. Fibres also increase the membrane life, compared to powder.

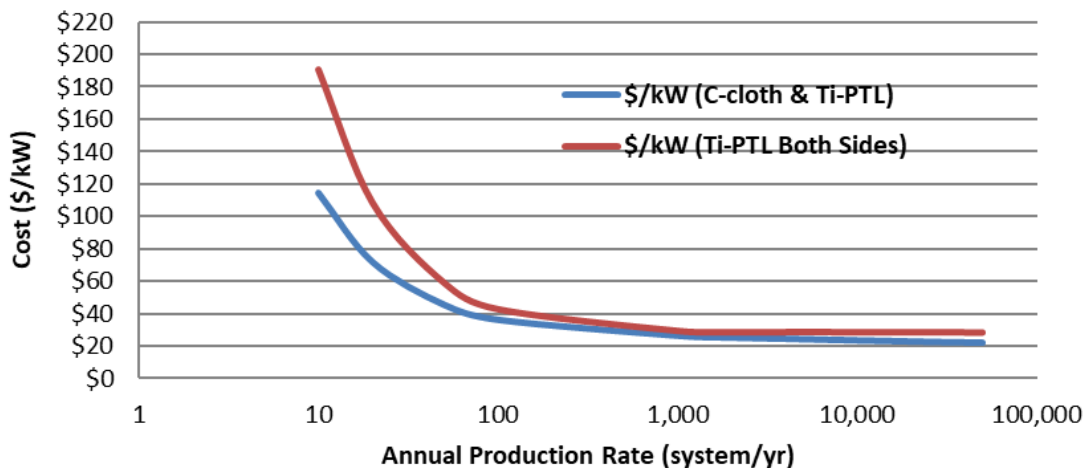


[https://www.researchgate.net/publication/333360045\\_Polymer\\_Electrolyte\\_Water\\_Electrolysis\\_Correlating\\_Performance\\_and\\_Porous\\_Transport\\_Layer\\_Structure\\_Part\\_II\\_Electrochemical\\_Performance\\_Analysis](https://www.researchgate.net/publication/333360045_Polymer_Electrolyte_Water_Electrolysis_Correlating_Performance_and_Porous_Transport_Layer_Structure_Part_II_Electrochemical_Performance_Analysis)  
<https://iopscience.iop.org/article/10.1149/2.0561904jes/pdf>

<https://www.semanticscholar.org/paper/Optimization-of-porous-current-collectors-for-PEM-Grigorieva-Baranova/28e162d1b4deb9e46fb14c3e0001085c62d4bf3e>

Using carbon or coated carbon felts instead of titanium powders, fibres and felts for the PTL can reduce cost.

## Carbon Cloth and Ti- Based PTL Cost



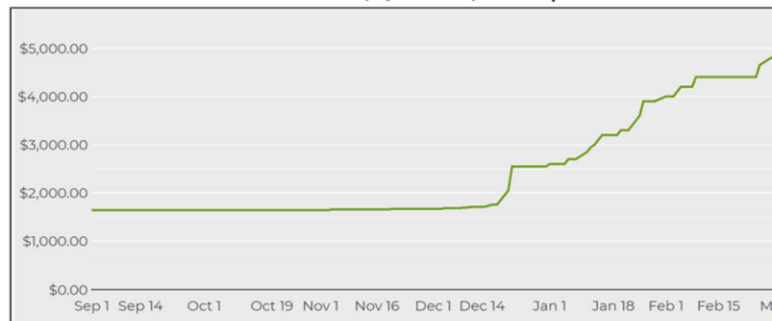
Freudenberg E35H carbon felt



Iridium oxide catalyses the oxygen evolution reaction. Avoidance of iridium oxide for the anode catalyst is possible, for example PMF powder from PAJARITO POWDER. But performance is reduced, and a larger membrane / electrolyser is required with additional materials usage.



Iridium Price, \$5800/toz April 2021



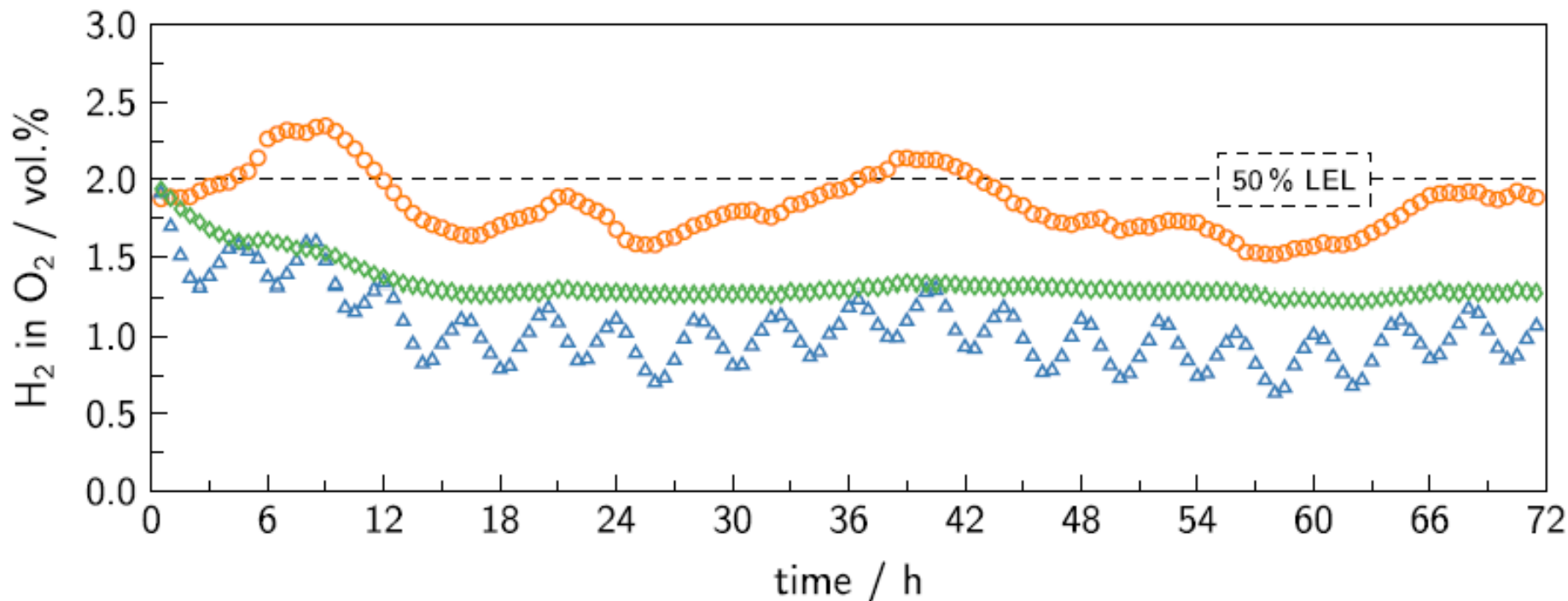
Platinum Price, \$1132/toz March 2021



# Innovations in PEM and alkaline electrolyser safety

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For alkaline electrolysis, the hydrogen in oxygen concentration can be 1.5%. 2% would be 50% of the LEL. For safety management and electrolyser process control, a measurement range of 0 to 5% may be suitable.



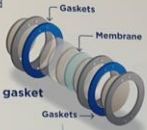
# SAINT-GOBAIN SOLUTIONS FOR THE

## PRODUCTION

COMPONENTS AND MATERIALS FOR ELECTROLYZERS

### PEM & ALKALINE ELECTROLYSIS

Zirconia active component for membranes and diaphragms

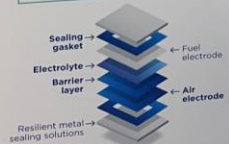


Fluoropolymer gasket for cell stacks



Insulating protection cover for pillars

### SOLID OXIDE ELECTROLYSIS



Processing materials and substrates for catalyst coated membranes (DECAL process)

**Ceramic solutions:**  
customized oxide powders and slurries,  
conductive ceramics, functional layers,  
cermet glass sealing, stack, module  
and system design

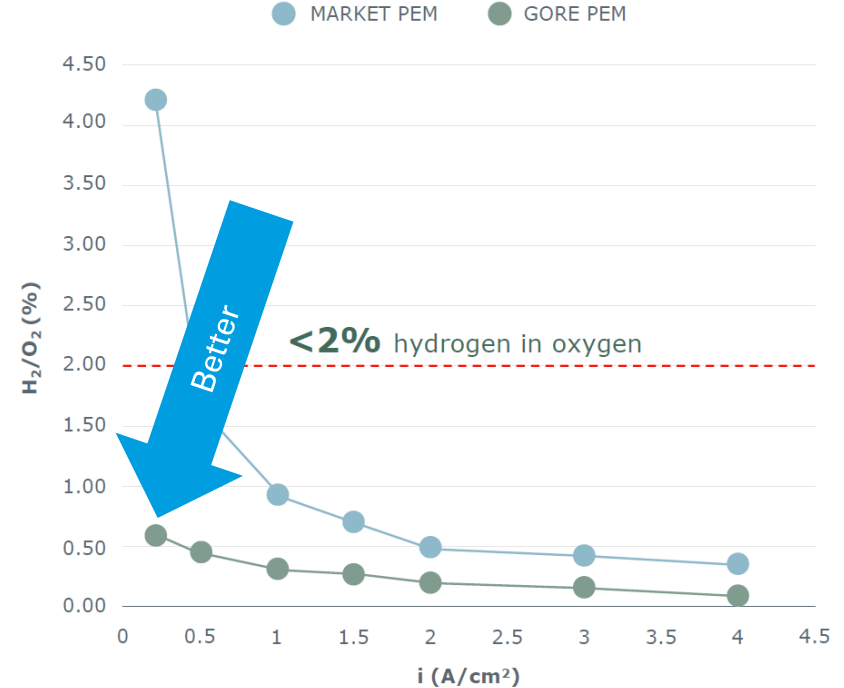
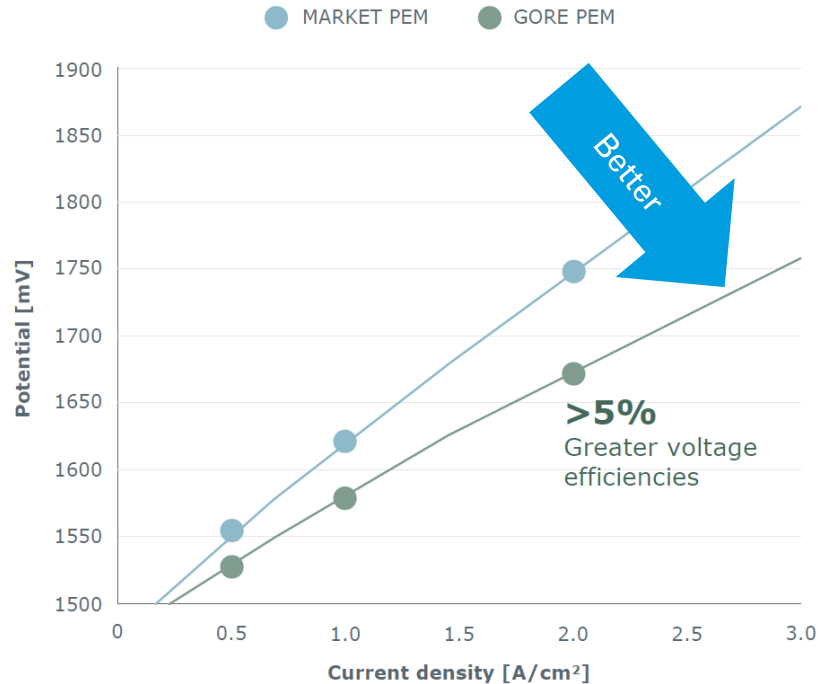
## TRANSPORT

STORAGE



sbh4  
consulting

Gore – making improvements to the polymer electrolyte membrane to reduce power input and improve operability at low-load conditions. Data presented is as expected for 80 °C, atmospheric pressure. This membrane is incorporated into the Siemens Energy Silyzer 300 stacks.





# Innovations in solid oxide electrolysis

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SOE – Solid Oxide Electrolysis

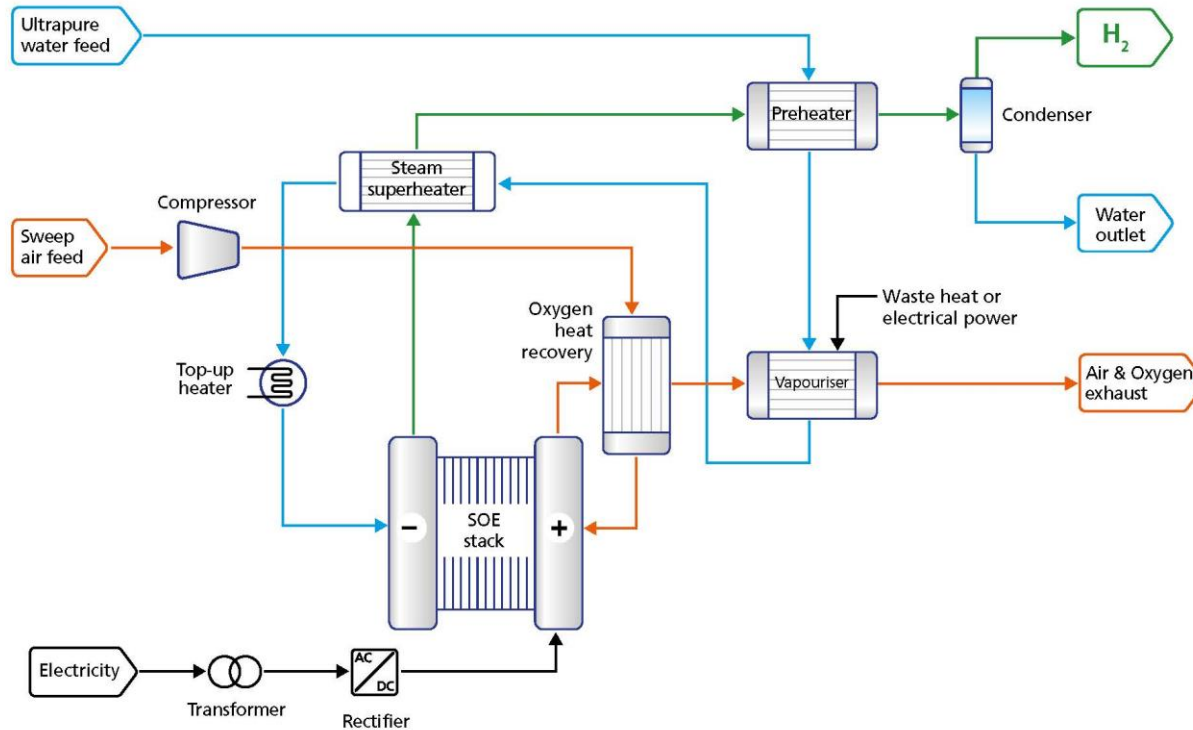
SOEC – Solid Oxide Electrolysis Cell

HTE – High Temperature Electrolysis

Co-SOEC / Co-electrolysis

CO<sub>2</sub> electrolysis / Electrolytic CO<sub>2</sub> reduction

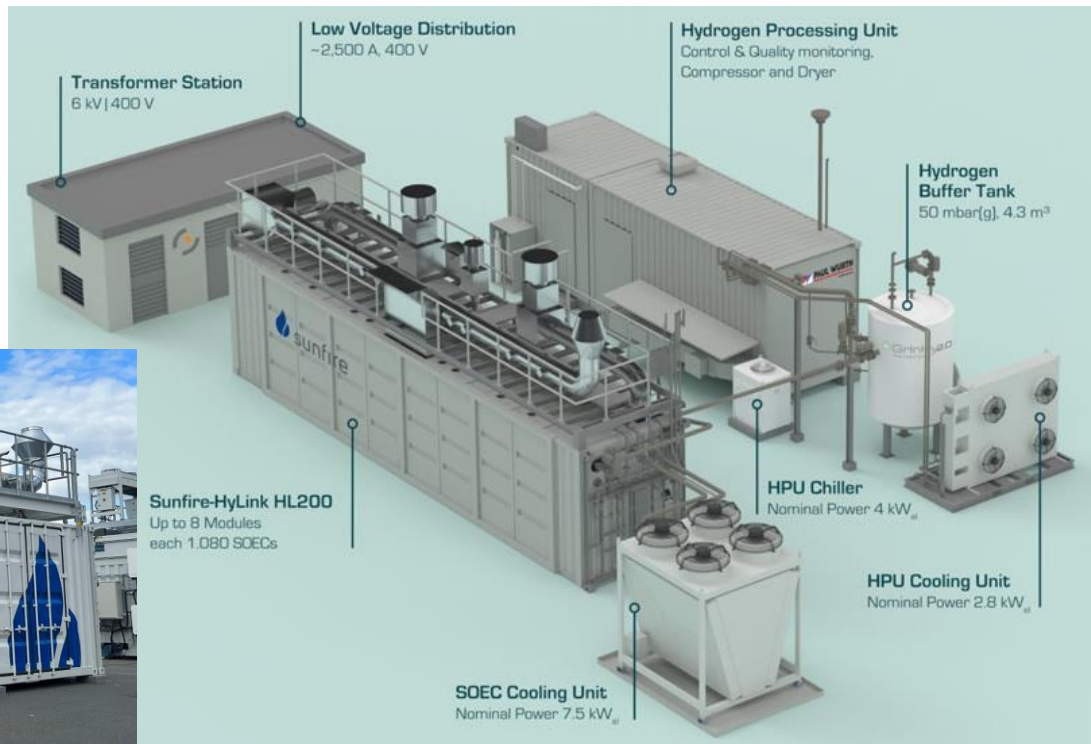
# Solid Oxide Electrolysis process for hydrogen generation



## SOEC for H<sub>2</sub> production

- With electrical steam generation, the system efficiency can be around 42 kWh / kg H<sub>2</sub>
- Waste heat can be used to vaporise the water feed and reduce the electrical power consumption
- With waste heat for steam, the system efficiency can be as good as 40 kWh / kg H<sub>2</sub> – about 20% better than many alkaline and PEM systems
- Low pressure hydrogen from the stack means compression and the associated capex and power is required, an additional 2 kWh/kg H<sub>2</sub> may be required to compress to circa 20 bar

# Sunfire – Solid Oxide Electrolysis for hydrogen production.



# FuelCell Energy: Solid Oxide Electrolysers in development, building on SOFC expertise.



- Capacity: 600 kg/day H<sub>2</sub> at atmospheric pressure
- H<sub>2</sub> purity (dry gas): 99% H<sub>2</sub>, 1%N<sub>2</sub>
- Power: 39.4 kWh/kg H<sub>2</sub> with steam input
  - Steam (up to): 146 °C, 3.2 bar, 258 kg/hr
- Power: 43.8 kWh/kg H<sub>2</sub> with water input
  - Water: 5,451 litres per day at < 1 µS/cm
- Footprint: 2x modules, each L40'xW8'xH10'
- Ramp rate: 10% per minute
- Flexibility: 0 to 100%

Ceres Power: Solid Oxide Electrolyser in demonstration at AVL Remscheid test centre, Germany. Further demonstration with Linde and BOSCH planned.

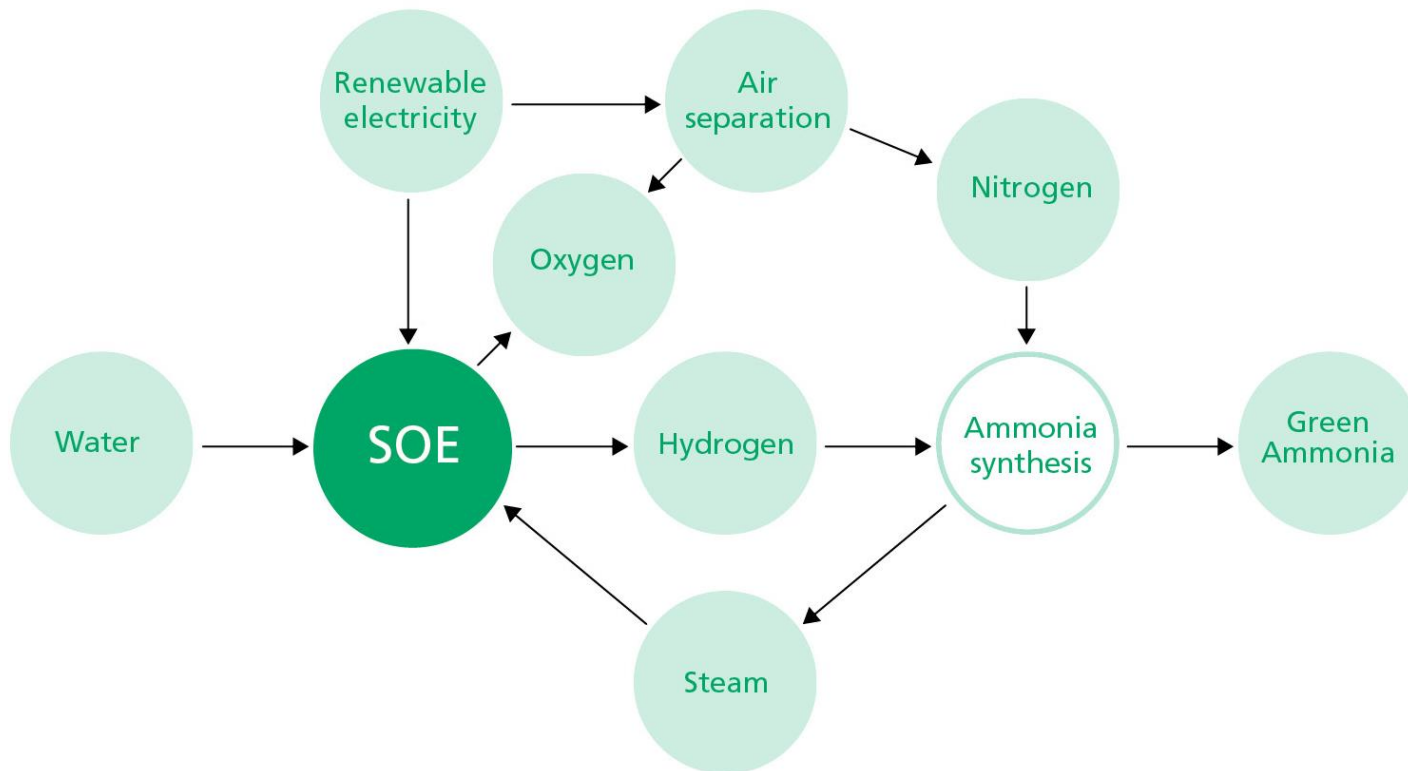
## Module Efficiency 38kWh/kg

Specification	Target Value
Electrical Power Input	100kW
Hydrogen Production	65kg / day
Module Efficiency	38kWh/kg
Steam input	150°C

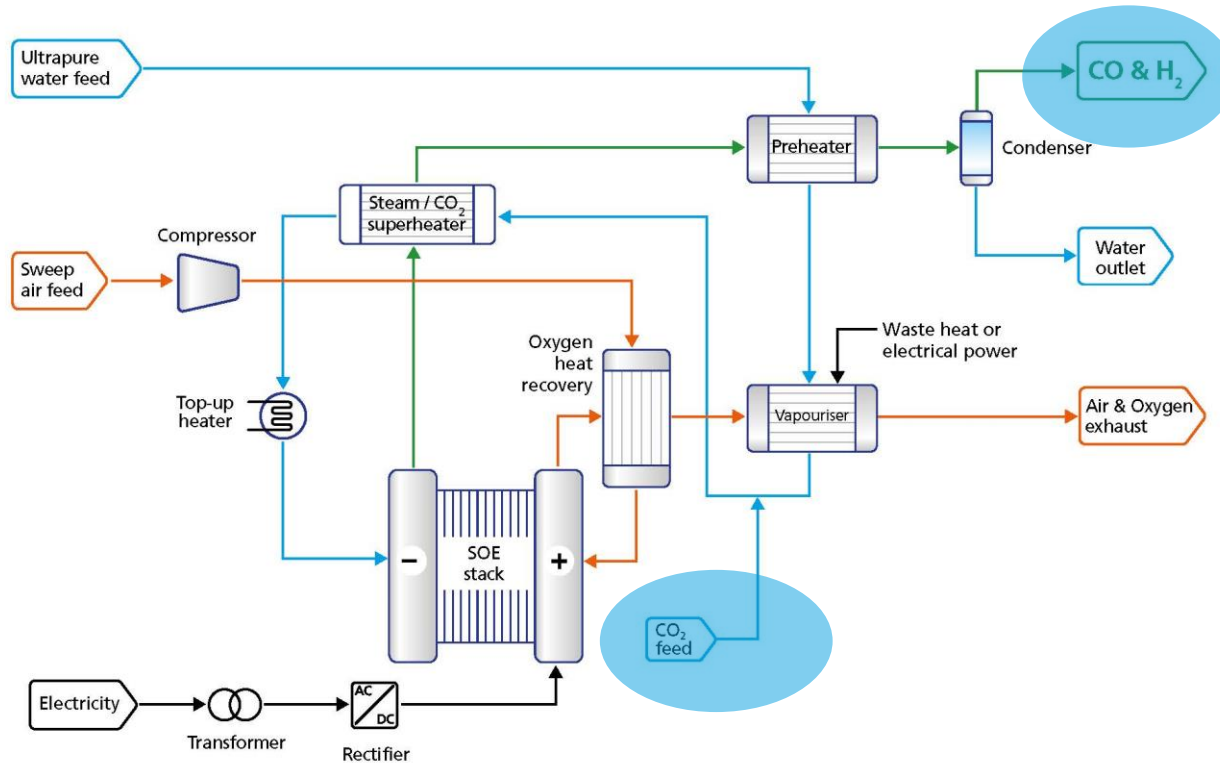




# SOEC for hydrogen integrates well with ammonia production.



# Solid Oxide Co-Electrolysis process for syngas generation



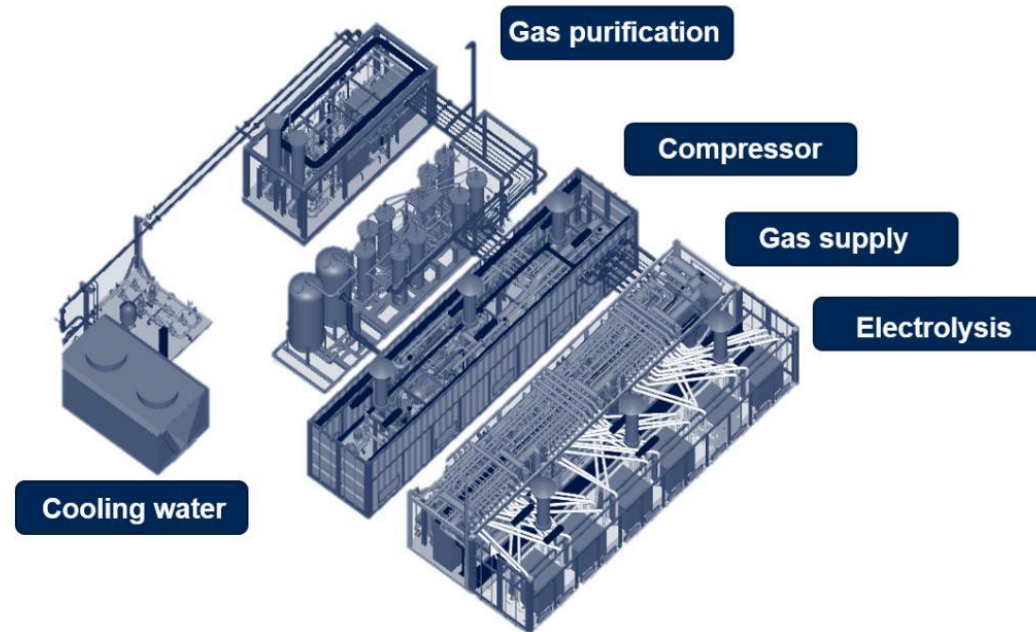
## Co-SOEC

- SOEC operating in Co-SOEC mode uses similar equipment to SOEC operating in steam to hydrogen mode
- The key difference is that high purity CO<sub>2</sub> is fed to the stack in addition to steam
- Syngas is produced
- For CO<sub>2</sub> reduction to CO (as Topsøe operates) only CO<sub>2</sub> is fed to the SOEC stack

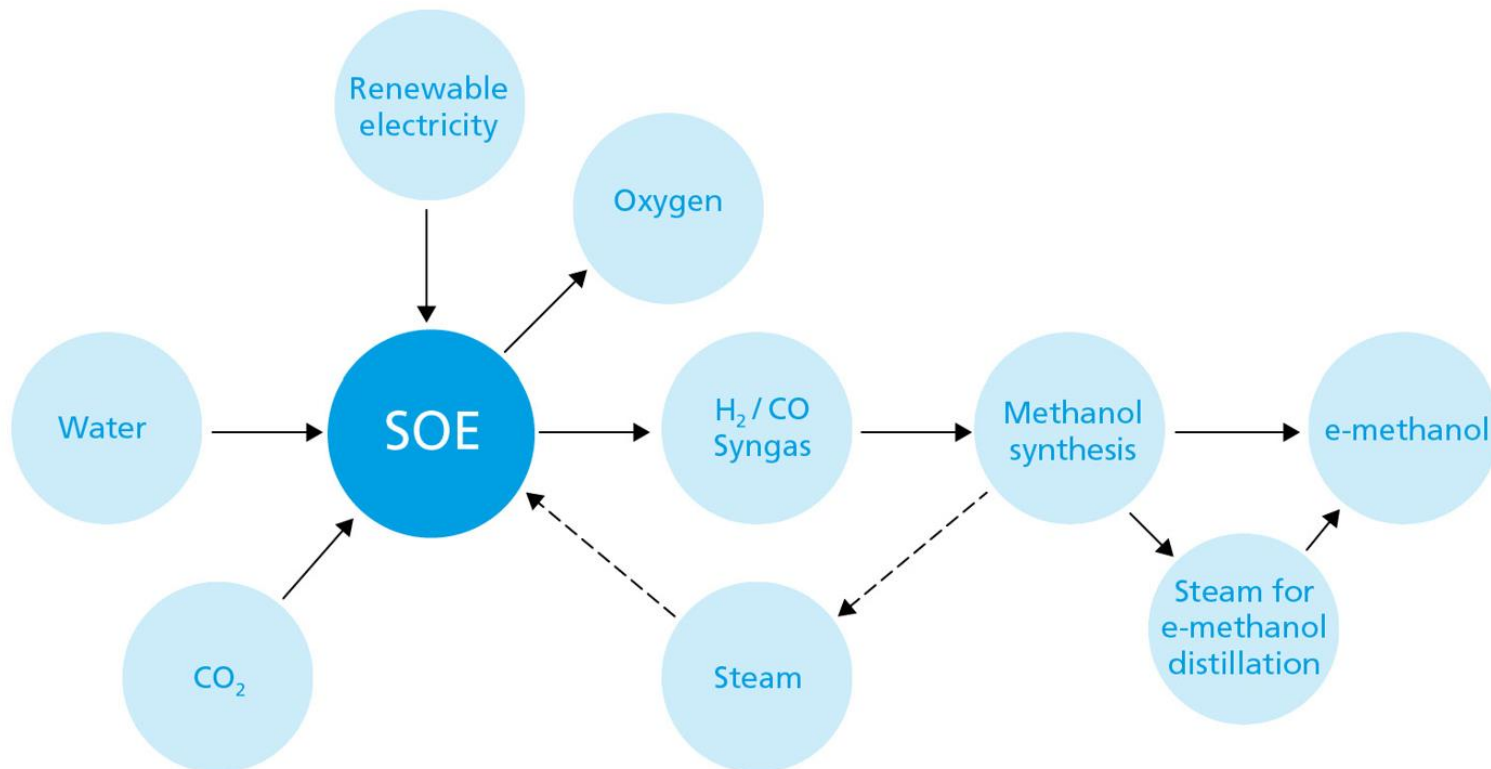
Topsøe eCOs™, CO<sub>2</sub> to CO reduction using electrolysis on SOEC. Topsøe leased 2 x 750 kW ultrapure CO<sub>2</sub> reduction CO production plants to DeLille Oxygen, USA.



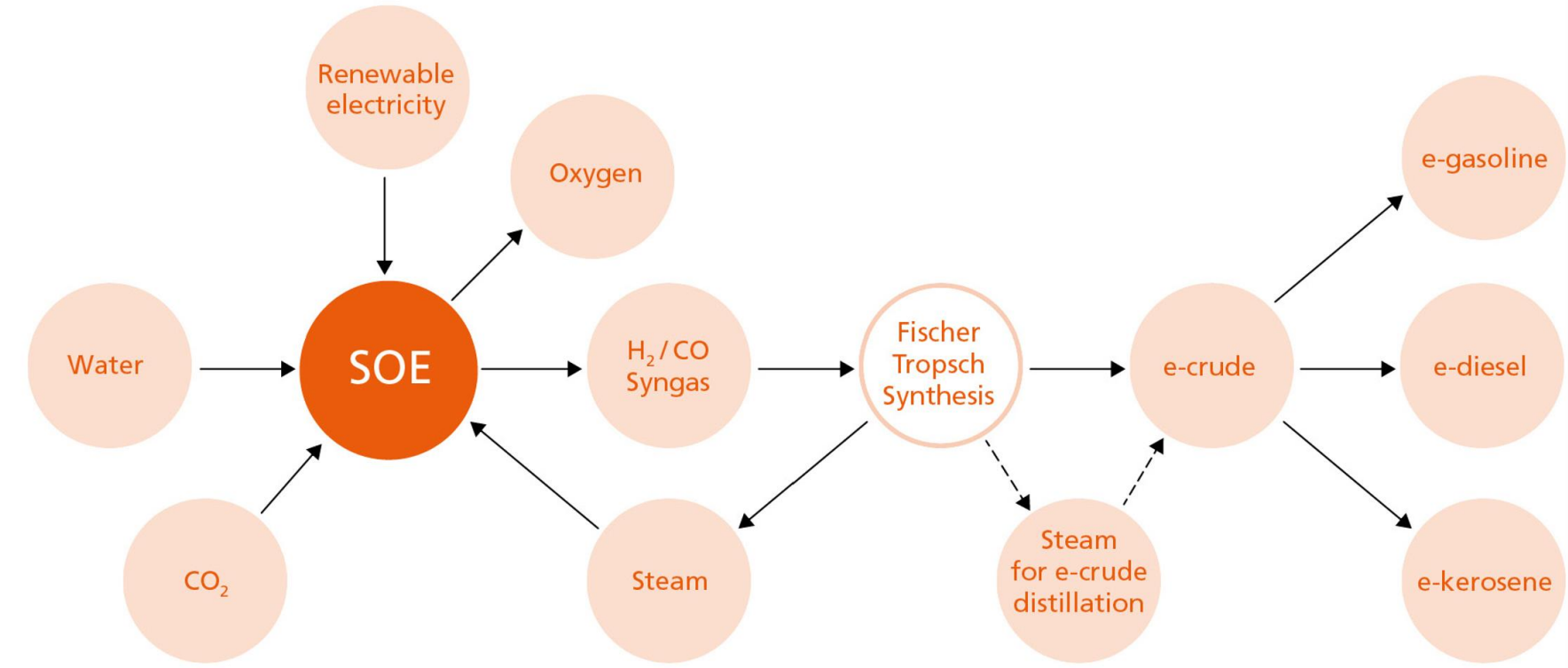
- Electrochemical process to enable green electrons to reduce CO<sub>2</sub> to CO
- CO can be combined with hydrogen to make syngas for methanol or FTS fuels



Co-SOEC for syngas production integrates well with e-methanol production. Some modern e-methanol plants use direct hydrogenation of CO<sub>2</sub>, avoiding the need to produce CO.



Co-SOEC for syngas production integrates well with Fischer Tropsch Synthesis (FTS) for Power to Liquids for e-fuels such as eSAF. Direct hydrogenation of CO<sub>2</sub> for FTS is being researched, but not yet deployed. So, syngas with CO and H<sub>2</sub> is required.





# Innovations in AEM electrolysis

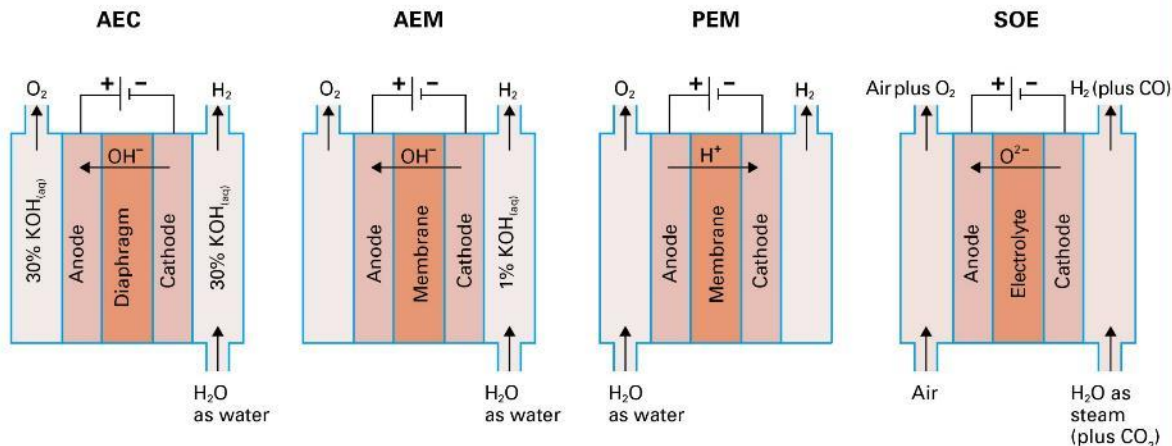
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AEM – Anion Exchange Membrane

AEM - Alkaline Electrolyte Membrane

## Notes:

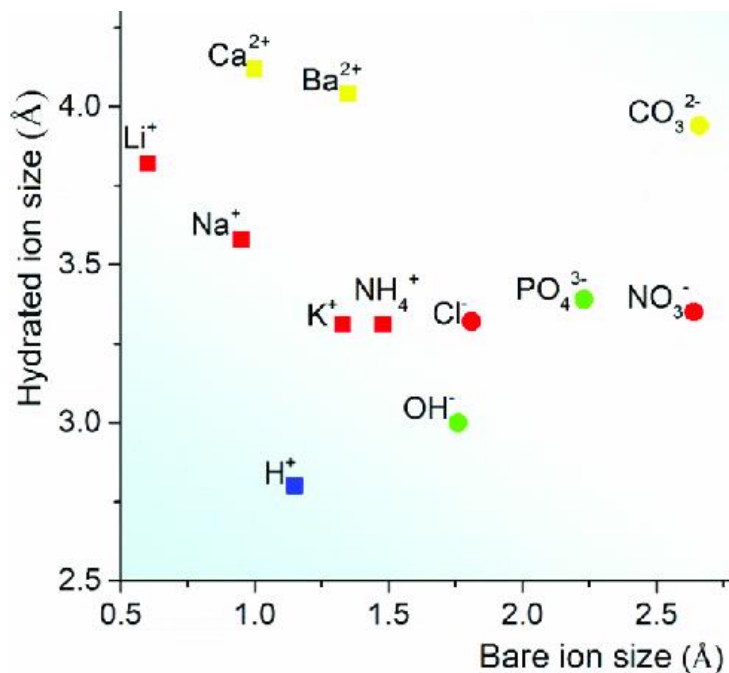
- In the AEC, AEM and PEM, lye or water flow from the electrolyser cell with the oxygen and/or hydrogen gases. These liquids are mixed and recirculated to the electrolyser.
- Air is used to purge the SOE anode to avoid oxygen accumulation which may present a hazard at the high operating temperature.
- Bipolar plates made of stainless steel (titanium for PEM) are used to stack adjacent cells in each electrolyser type.



	Alkaline Electrolysis Cell AEC	Anion Exchange Membrane / Alkaline Electrolyte Membrane AEM	Polymer Electrolyte Membrane/ Proton Exchange Membrane PEM/PEMEC	Solid Oxide Electrolysis Cell SOE/SOEC
Electrode material	– Cathode: Ni, Co or Fe – Anode: Ni	– Cathode: Ni / Ni alloys – Anode: Fe, Ni, Co oxides	– Cathode: Pt/Pd – Anode: IrO <sub>2</sub> /RuO <sub>2</sub>	– Cathode: Ni – Anode: La/Sr/MnO (LSM) or La/Sr/Co/FeO (LSCF)
Electrolyte	Lye: 25-30% Potassium Hydroxide solution in water	Anion Exchange ionomer (e.g. AS-4)	Fluoropolymer ionomer (eg Nafion, a DuPont brand)	Zirconium Oxide with ~8% Yttrium Oxide
Energy source	100% electrical power	100% electrical power	100% electrical power	~25% heat from steam, ~75% electrical power
Current density	Up to 0.5 A/cm <sup>2</sup>	0.2 – 1 A/cm <sup>2</sup>	Up to 3 A/cm <sup>2</sup>	Up to 0.5 A/cm <sup>2</sup>
Hydrogen or syngas product	Hydrogen	Hydrogen	Hydrogen	Hydrogen (or syngas if fed with steam and CO <sub>2</sub> )
Gas outlet pressure	Up to 40 bar	Up to 35 bar H <sub>2</sub> , 1 bar O <sub>2</sub>	Up to 40 bar	Close to atmospheric
Cell temperature	~80 °C	~60 °C	~60 °C	~750 to 850 °C

- AEM sits between alkaline (AEC) and PEM technologies
- Operating conditions are alkaline like AEC, not acidic like PEM
- Materials of construction and catalysts are low-cost, like AEC
- System has potential to be low capex
- The use of a membrane gives it characteristics close to PEM technology
- AEM aligns well with intermittent operation and variable renewable power input
- Efficiencies are not yet as good as most PEM or alkaline systems
- Key development in recent years has been to increase the stack life with improved membrane durability

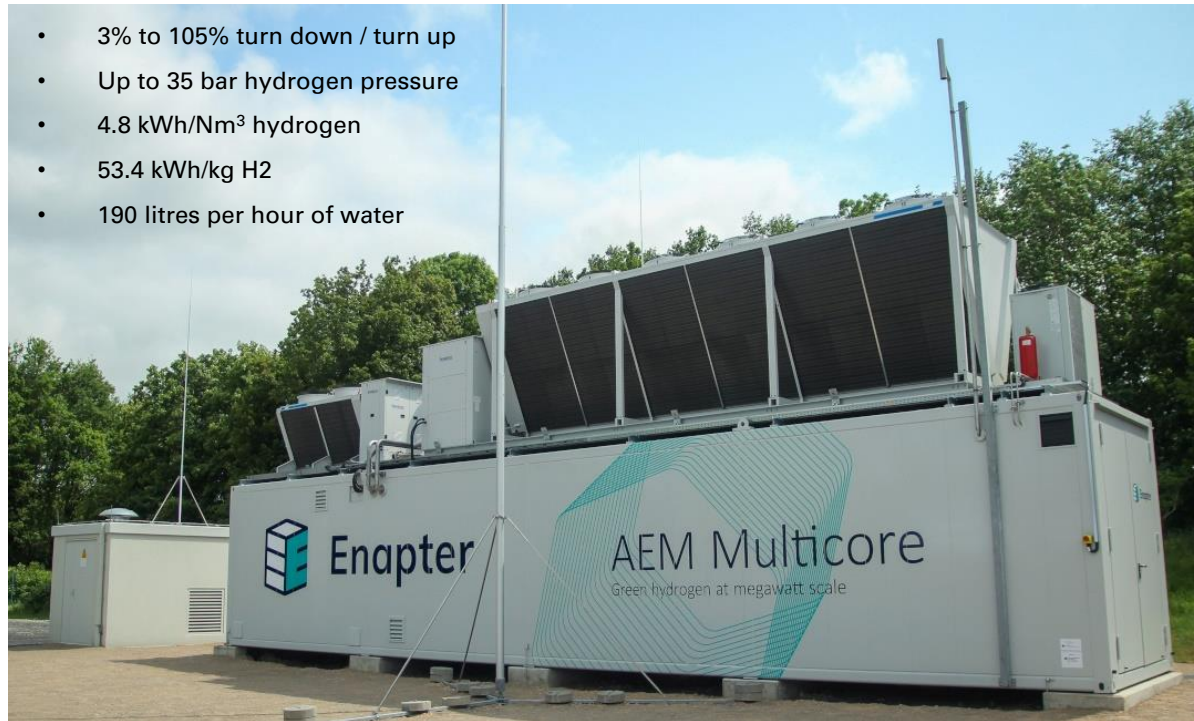
Shooting an OH<sup>-</sup> ion through a membrane is like Dirty Harry firing a Smith & Wesson model 29 bullet at a punk.



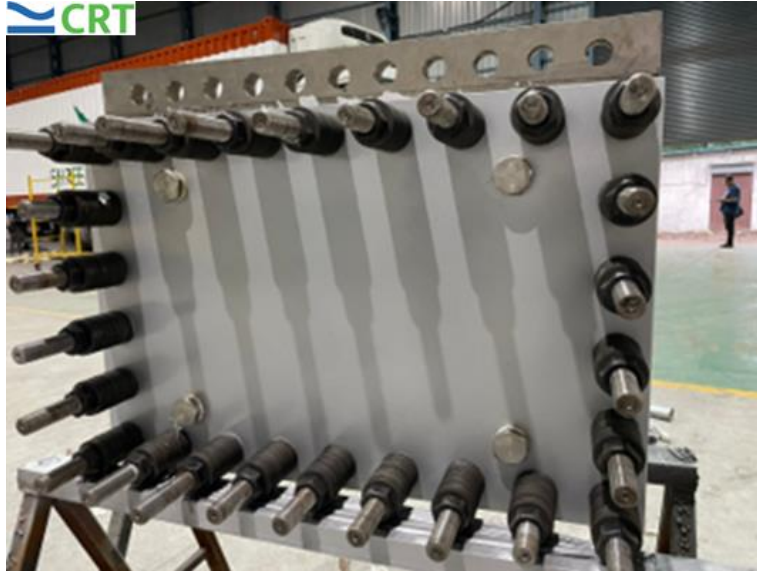


# Enapter AEM Nexus, 1MW Multicore (420 modules) at Bioenergiepark Saerbeck. 210 Nm<sup>3</sup>/hr (450 kg / day) of hydrogen at 99.9% purity (99.999% with dryer).

- 3% to 105% turn down / turn up
- Up to 35 bar hydrogen pressure
- 4.8 kWh/Nm<sup>3</sup> hydrogen
- 53.4 kWh/kg H<sub>2</sub>
- 190 litres per hour of water



Cavendish Renewable Technology – large AEM stack in development.  
Membrane life is extended using low temperature operation, enabled by innovative membrane catalyst coating.





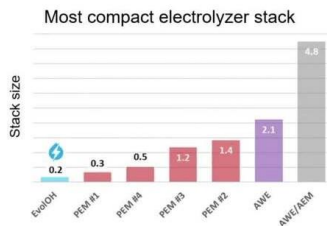
**EVōLOH – Carbonate AEM electrolysis. Membrane life is extended using buffered electrolyte with pH close to 7. Focus on stack production at scale and low cost. Allow EPCs to integrate the stacks into large systems.**



**Our customer**

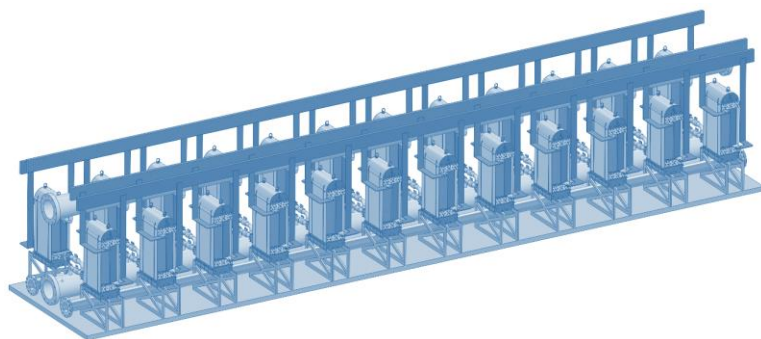
No corrosive liquids	→	Cheaper water mgmt. unit
Pressurized H <sub>2</sub>	→	Cheaper compression units
Compact units	→	Cheaper shipping & installation
Standard power requirement	→	Cheaper & widely available power supplies

...and more



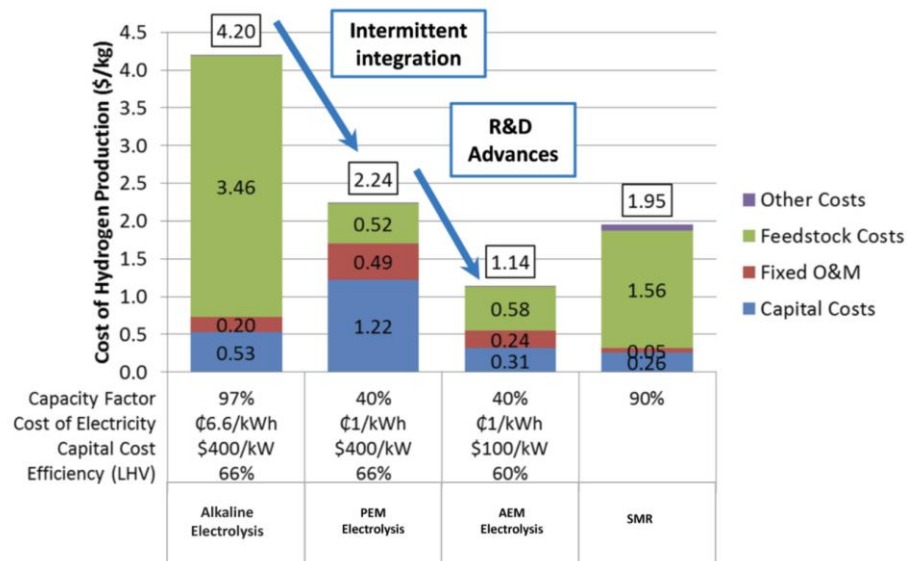
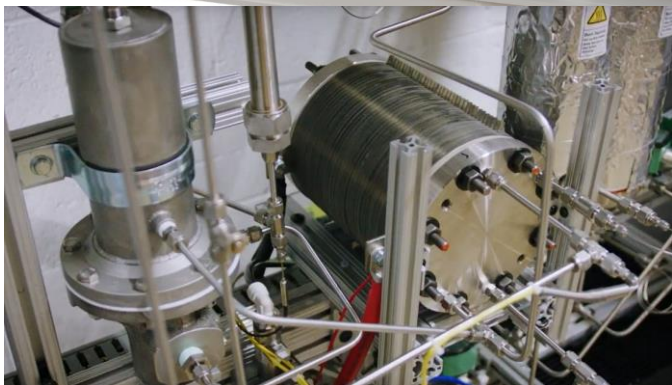
At least 50% higher power density compared to best state-of-the-art PEM

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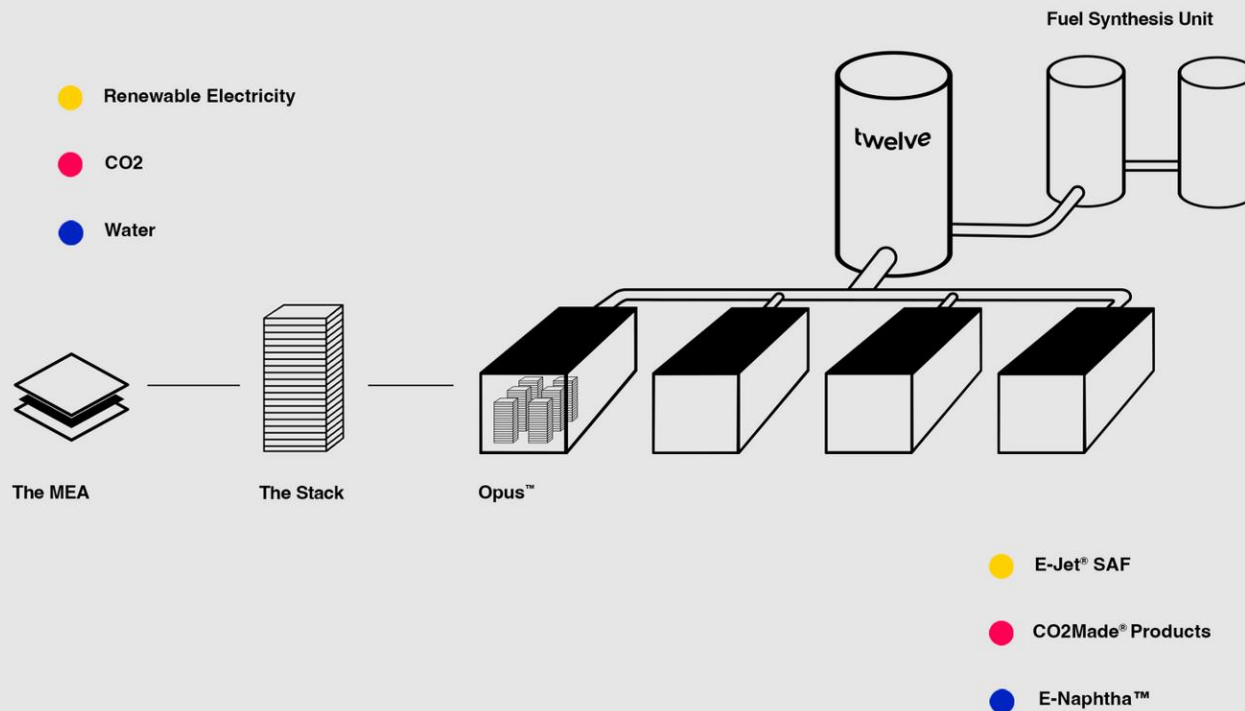
- Low-cost stack materials: aluminium, plastic, steel and carbon
- Targeting USD30 per kW for stacks (excludes BOP)
- IP surrounding the electrodes and electrode materials
- Highly manufacturable stack
- Reel to reel manufacturing
- 3.75 GW per year stack production planned
- High power density to reduce stack size
- Membrane life extended due to use of less aggressive carbonate electrolyte with pH close to 7

# High pressure AEM with 200 bar hydrogen for ammonia or hydrogen mobility. POWER to HYDROGEN (P2H2) Clean Energy Bridge™.

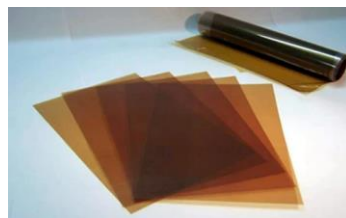
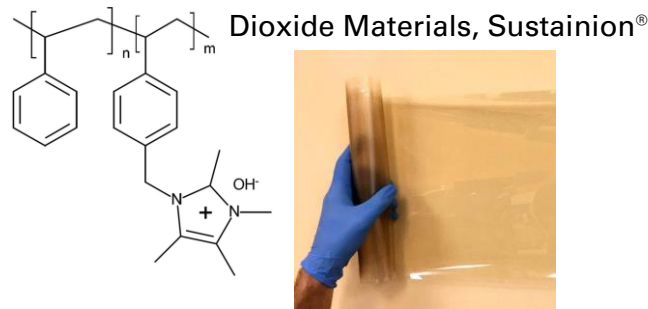


- 200 bar hydrogen generation
- Pure oxygen co-generation
- Able to integrate with variable renewables

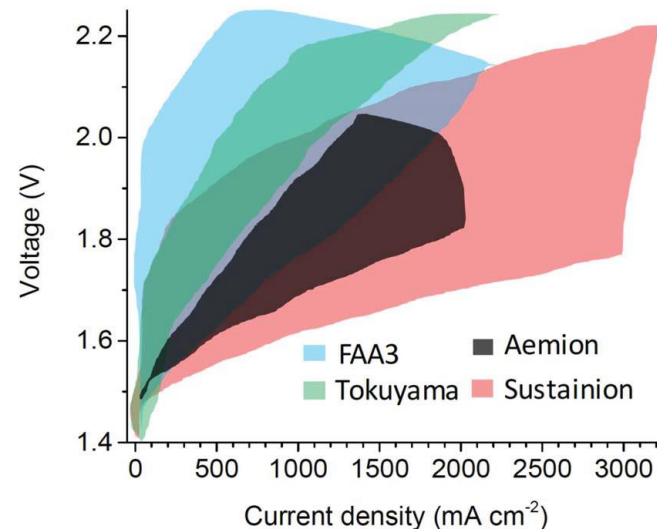
# Twelve, USA. Using AEM-type electrolysis to convert water and CO<sub>2</sub> to syngas for hydrocarbon production.



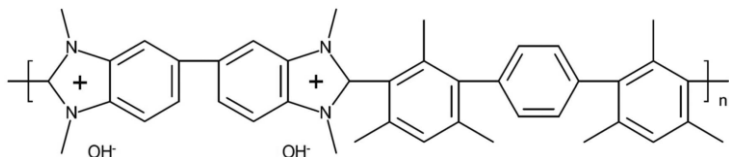
# Ionomr Innovations and several others developing 'fluoropolymer-free' AEM membranes.



Fumatech, Fumasep FAA-3



Ionomr Innovations, Aemion+™



[https://asmedigitalcollection.asme.org/electrochemical/article-pdf/18/2/024001/6673712/jeeecs\\_18\\_2\\_024001.pdf](https://asmedigitalcollection.asme.org/electrochemical/article-pdf/18/2/024001/6673712/jeeecs_18_2_024001.pdf)

<https://ionomr.com/solutions/aemion/>

<https://dioxidematerials.com/product/40-micron-sustainion-x37/>

<https://www.laborxing.com/de/products/fumasep-faa-3-pk-130-anion-exchange-membrane#>



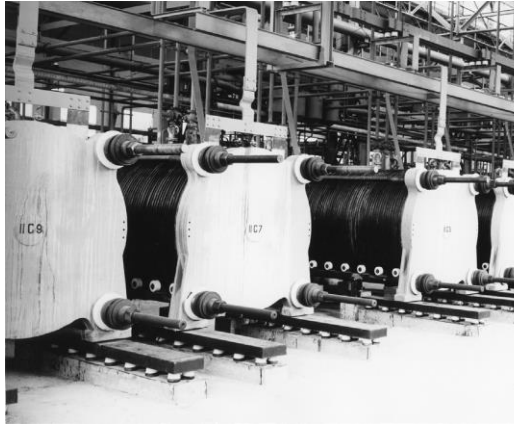
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# Innovation or chaos?

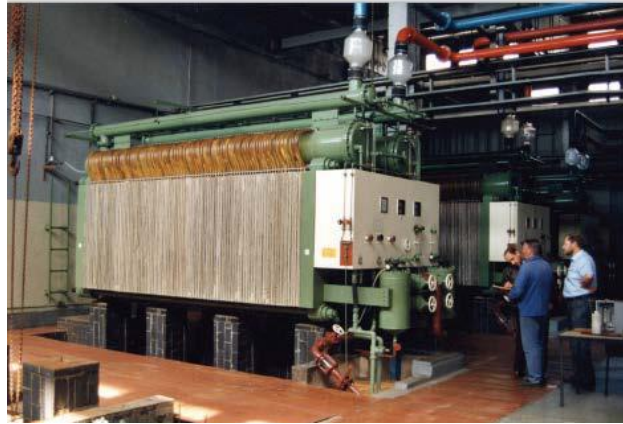
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Alkaline electrolysis from hydropower for green hydrogen has been deployed in Norway, Egypt and Zimbabwe at 100+ MW since 1928. The target molecule in each case was ammonium nitrate. In the 1970s, cheap grey hydrogen / grey ammonia from natural gas reforming made all these facilities uneconomical.



- 1949
- Hydro power from Glomfjord, Norway
- Ammonium nitrate fertilizer production
- Nel alkaline electrolysis
- 160 MW on 150 modules
- 27,100 Nm<sup>3</sup> / hr H<sub>2</sub> at atmospheric pressure



- 1973
- Kima Fertilizer plant, Egypt
- Hydro power from the Aswan dam
- BBC Electrolyzer System Oerlikon
- 144 MW alkaline electrolysis (144 modules)
- 32,000 Nm<sup>3</sup> / hr hydrogen at atmospheric pressure



- 1973
- Sable Chemicals ammonia plant, Kwekwe, Zimbabwe,
- Hydro power from the Kariba dam
- Electrolysers from Lurgi, (now Sunfire, through IHT acquisition)
- 100MW Pressurised Alkaline (28 x 3.5MW)
- 21,000 Nm<sup>3</sup> / hr hydrogen at 30 bar
- Hydrogen for Ammonia source switched to rail imports from South Africa in 2015, electrolyzers no longer in use

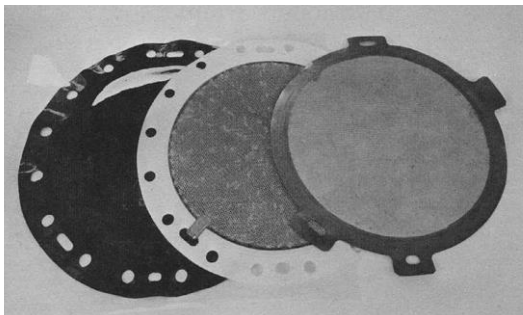
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<https://hydrogenoptimized.com/history/>

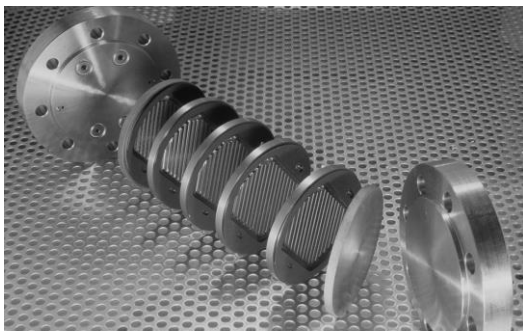
[https://www.google.com/url?sa=t&rct=j&q=&esrc=s&source=web&cd=&ved=2ahUKEwjZgbDz7Yv2AhUJH0wKHVKiBIEQFnoECAYQAQ&url=http%3A%2F%2Fwww.elygrid.com%2Fwp-content%2Fuploads%2F2021%2F07%2Fevent\\_8th-international-symposium-hydrogen-and-energy.pdf&usq=A0vVaw38Uh2oRsQgsfPBsl54mifu](https://www.google.com/url?sa=t&rct=j&q=&esrc=s&source=web&cd=&ved=2ahUKEwjZgbDz7Yv2AhUJH0wKHVKiBIEQFnoECAYQAQ&url=http%3A%2F%2Fwww.elygrid.com%2Fwp-content%2Fuploads%2F2021%2F07%2Fevent_8th-international-symposium-hydrogen-and-energy.pdf&usq=A0vVaw38Uh2oRsQgsfPBsl54mifu)

Image from NEL Hydrogen, published in Hydrogen Production by Water Electrolysis, Copyright Elsevier 2022

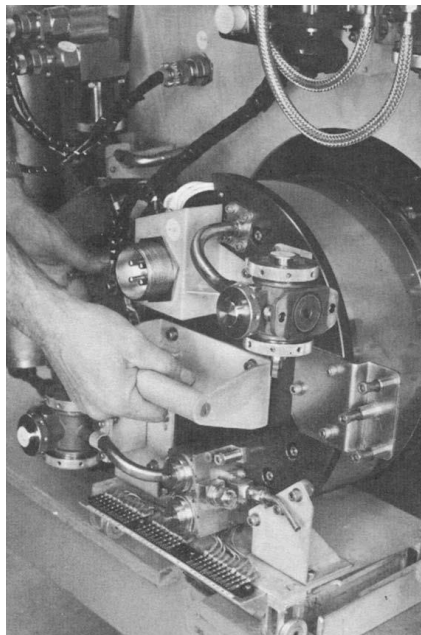
Early PEM (SPE) electrolyzers were developed for oxygen supply on US Navy nuclear submarines to enable long dives. They were also used in space stations to convert water to oxygen. MW-scale PEM-based green hydrogen concepts were developed in the 1970's.



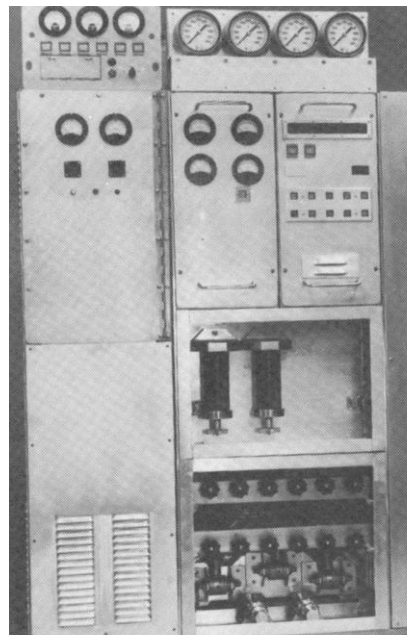
General Electric Company PEM (Solid Polymer Electrolyte, SPE) cell, late 1960s



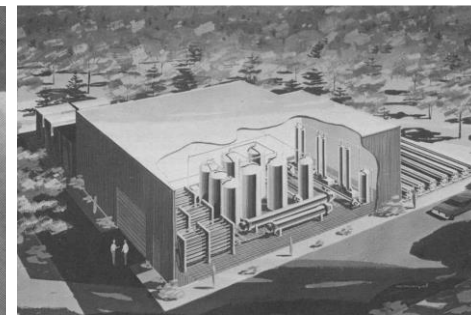
Siemens PEM stack, 1989



NASA 27-cell PEM stack, late 1960s



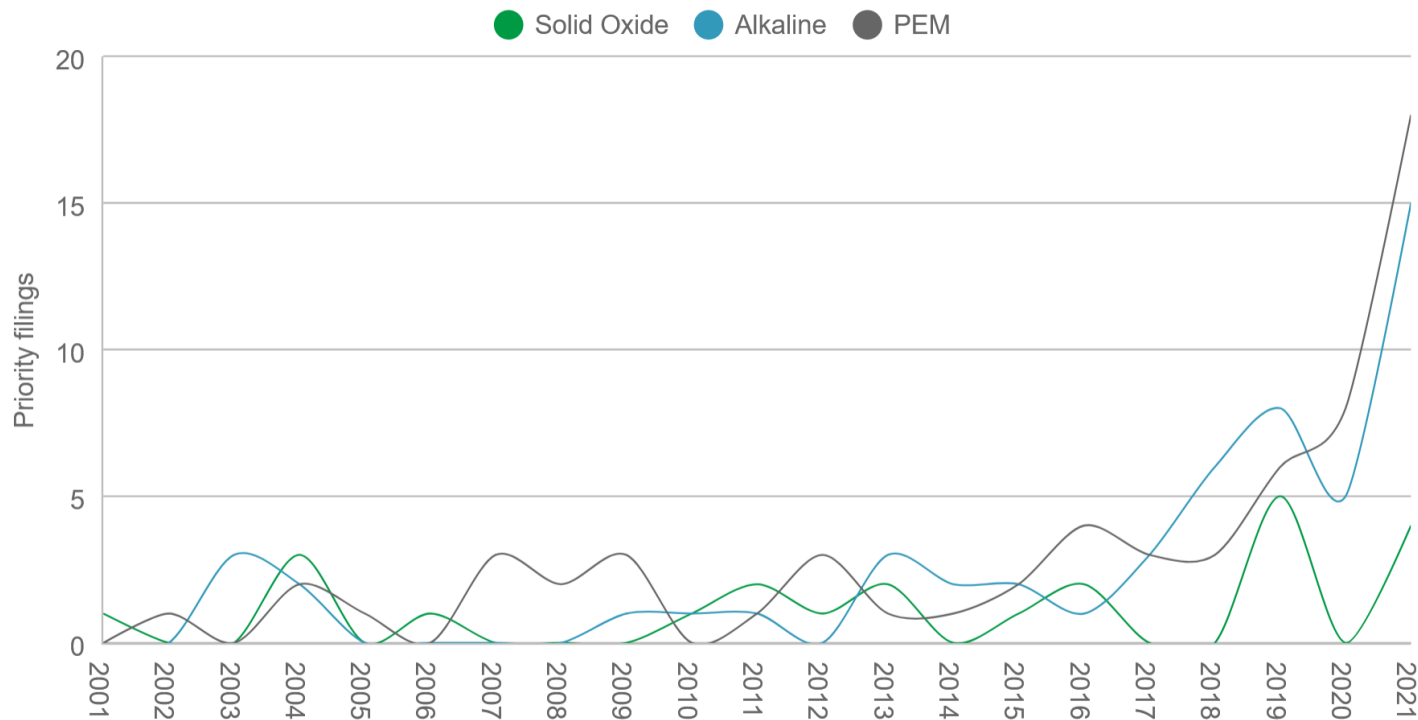
General Electric Company PEM electrolyser to produce oxygen for US navy submarines, late 1970s



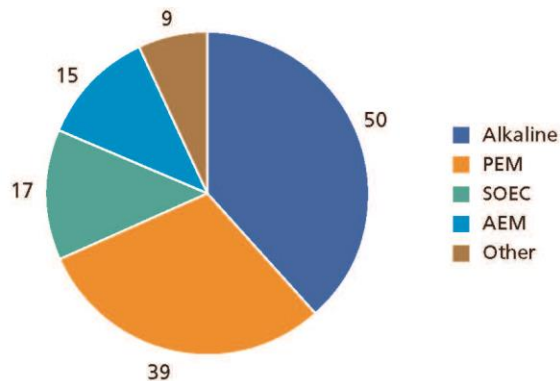
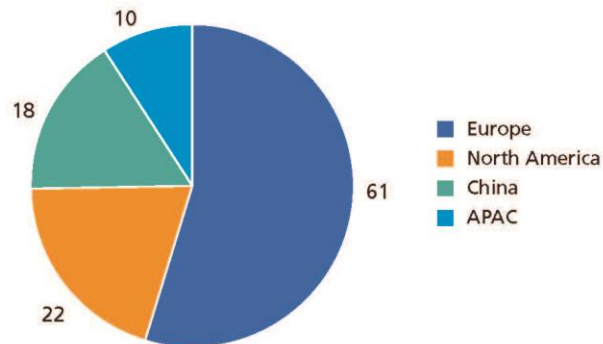
General Electric Company 73MW PEM green hydrogen conceptual plant

CONCEPTUAL DESIGN OF LARGE SCALE WATER ELECTROLYSIS PLANT USING SOLID POLYMER ELECTROLYTE TECHNOLOGY, L. J. NUTTALL, General Electric Company, 1977  
STATUS OF SOLID POLYMER ELECTROLYTE FUEL CELL TECHNOLOGY AND POTENTIAL FOR TRANSPORTATION, APPLICATIONS, L. J. NUTTALL, General Electric Company, 1983  
Siemens image from Hydrogen Production by Water Electrolysis, Tom Smolinka and Jürgen Garche

Alkaline and PEM electrolyser technologies are still innovating, as shown by patent filings in 2021. Will AEM and SOEC catch up through this decade?



# Electrolyser producers and emerging players



## Notes

Numbers shown are number of players as of March 2024

APAC data excludes China

In the technology split, some players feature more than once

Alkaline includes pressurised and atmospheric pressure

**PEM** – Proton Exchange Membrane

**SOEC** – Solid Oxide Electrolysis

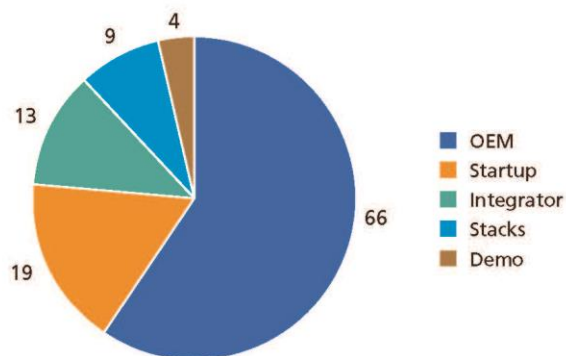
**AEM** – Anion Exchange Membrane

**OEM** – Commercial electrolyser production

**Integrator** – purchasing stacks and building systems

**Stacks** – focused on stack production, not systems

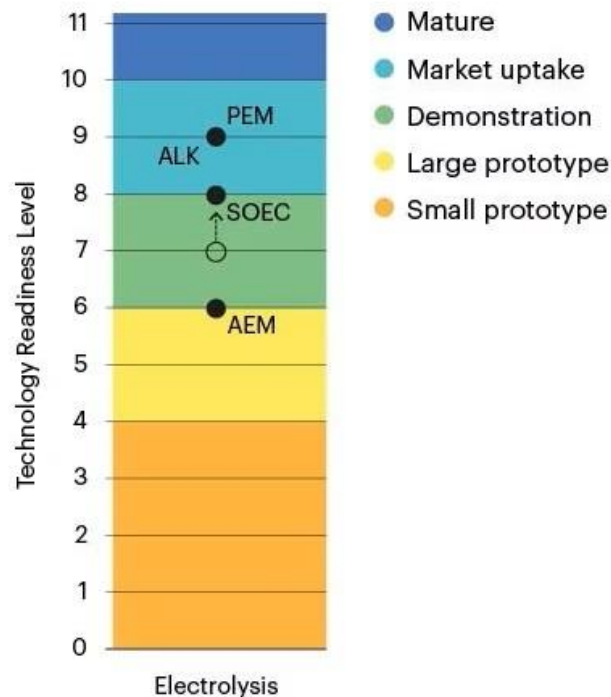
**Demo** – first commercial demonstration achieved



- Data that sbh4 tracks has shown a rapid growth in AEM and SOEC technology providers and startups
- AEM or SOEC startups may need 3 to 5 years to develop a commercial stack and system
- Many new PEM and Alkaline OEMs are also emerging rapidly
- Alkaline and PEM startups may need 2 to 3 years to develop a commercial offer and establish the required supply chain



Beware over-simplification! Alkaline and PEM are often declared to be mature technologies with a high TRL. Ok, so...if a new PEM or alkaline electrolyser producer emerges in 2024 using an innovative stack or system, is **their** technology, product and manufacturing mature? Or what about a new factory with new people and equipment?





TRL is only partially meaningful at this stage of PEM and alkaline electrolyser production scale up. TRL was developed to assess aerospace systems that were never designed to be mass-produced, nor was cost the major focus. DFMA is critical to ensure success and MRL may be a relevant scale.

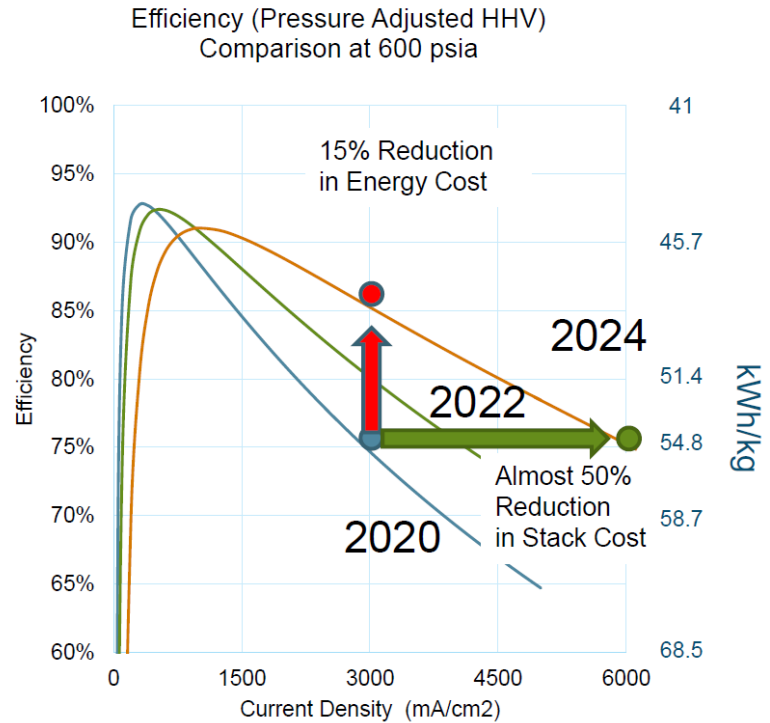
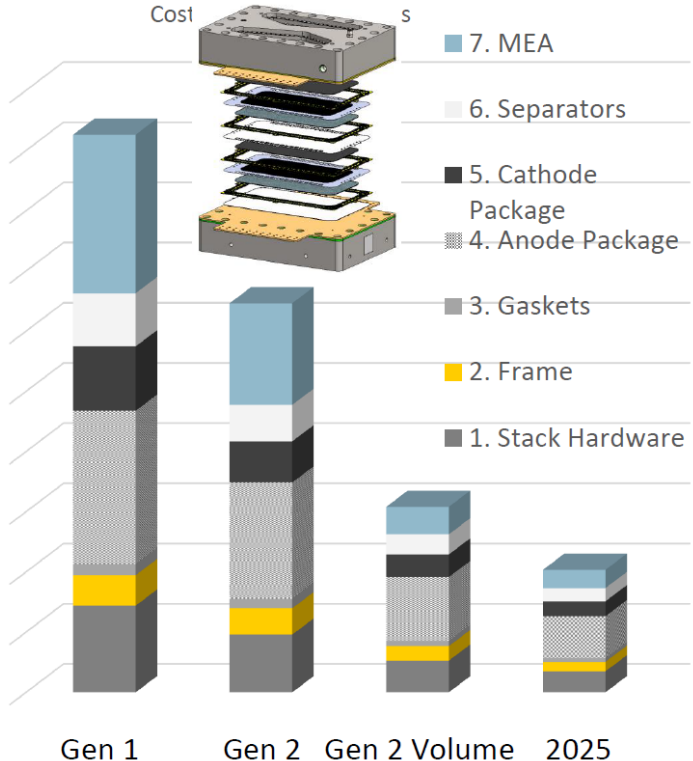
TRL 9	Actual system “flight proven” through successful mission operations
TRL 8	Actual system completed and “flight qualified” through test and demonstration (ground or space)
TRL 7	System prototype demonstration in a space environment
TRL 6	System/subsystem model or prototype demonstration in a relevant environment (ground or space)
TRL 5	Component and/or breadboard validation in relevant environment
TRL 4	Component and/or breadboard validation in laboratory environment
TRL 3	Analytical and experimental critical function and/or characteristic proof-of-concept
TRL 2	Technology concept and/or application formulated
TRL 1	Basic principles observed and reported

Phases	MRL	Definition
Operations and Support	10	Full Rate Production demonstrated and lean production practices in place.
Production and Deployment	9	Low Rate Production demonstrated. Capability in place to begin Full Rate Production.
Engineering and Manufacturing Development	8	Pilot line capability demonstrated. Ready to begin low rate production.
	7	Capability to produce systems, subsystems or components in a production representative environment.
Technology Development	6	Capability to produce a prototype system or subsystem in a production relevant environment.
	5	Capability to produce prototype components in a production relevant environment.
Material Solutions Analysis	4	Capability to produce the technology in a laboratory environment.
	3	Manufacturing proof of concept developed
	2	Manufacturing concepts identified
	1	Basic manufacturing implications identified

# Innovations in electrolyser manufacturing

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Plug Power: manufacturing cost reductions from stack design changes, reduced materials wastage and manufacturing automation leading to 75% labour input reduction. Efficiency improvements achieved in parallel.



Larger PEM stacks are converging to circa 1MW with a rectangular cell shape. Compared to a circular cell shape, the rectangular shape minimises wasted materials during manufacture and reduces cost.





Stiesdal, Denmark. Nitrogen shrouded, pressurised alkaline electrolyser. Rectangular stack produced by Danfoss. Standardised 3MW HydroGen unit with 46 to 49 kWh/kg H<sub>2</sub> efficiency. Target electrolyser **system** capex €200 per kW of power.





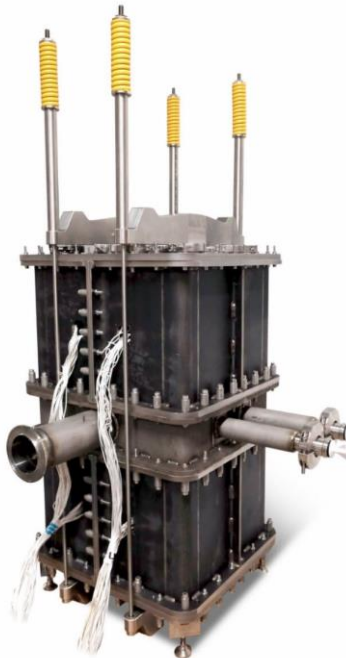
# Innovation in electrolyser supply chains

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2JCP– providing systems integration engineering services to Siemens Energy to build Silyzer 300 systems in the Czech Republic around the PEM stacks produced in Germany. This shipment ready for European Energy in Kassø.

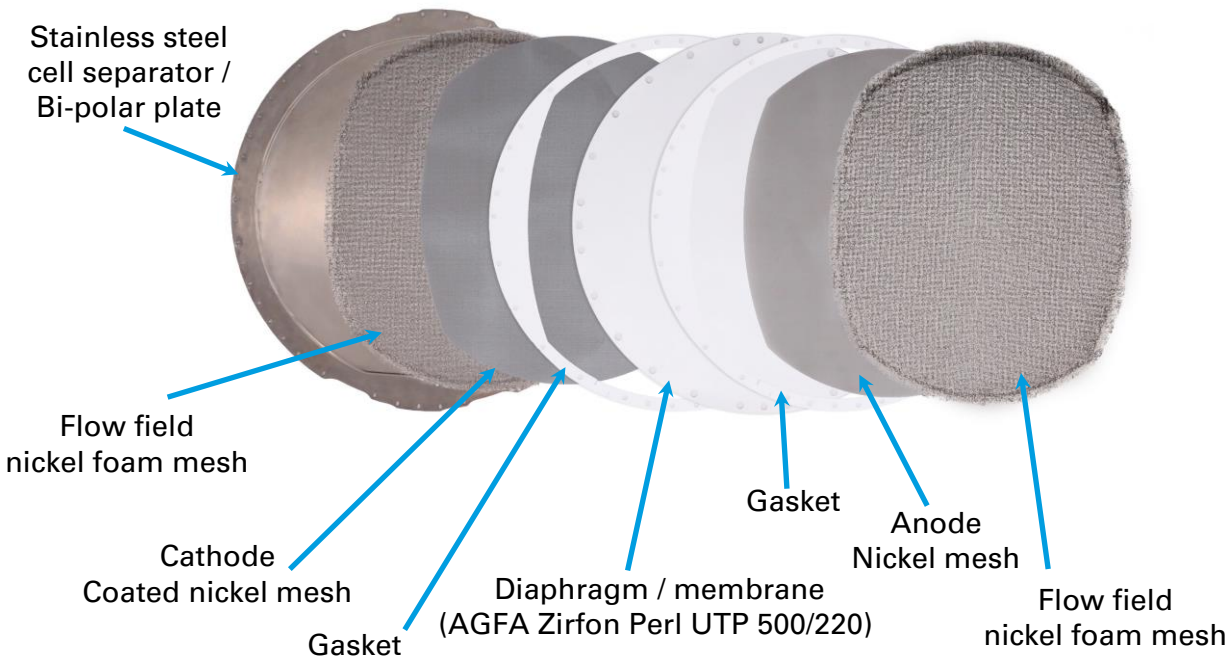


# Convion integrating Elcogen elcoStack 3000 SOEC stack modules into full electrolyser systems.

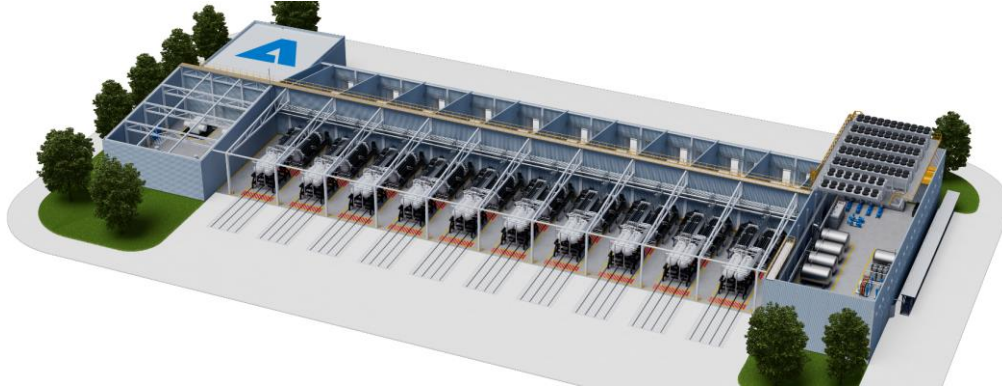




# McPhy and De Nora technology partnership. Alkaline cell with 8-layer architecture and components. Used in McPhy PA electrolyzers.

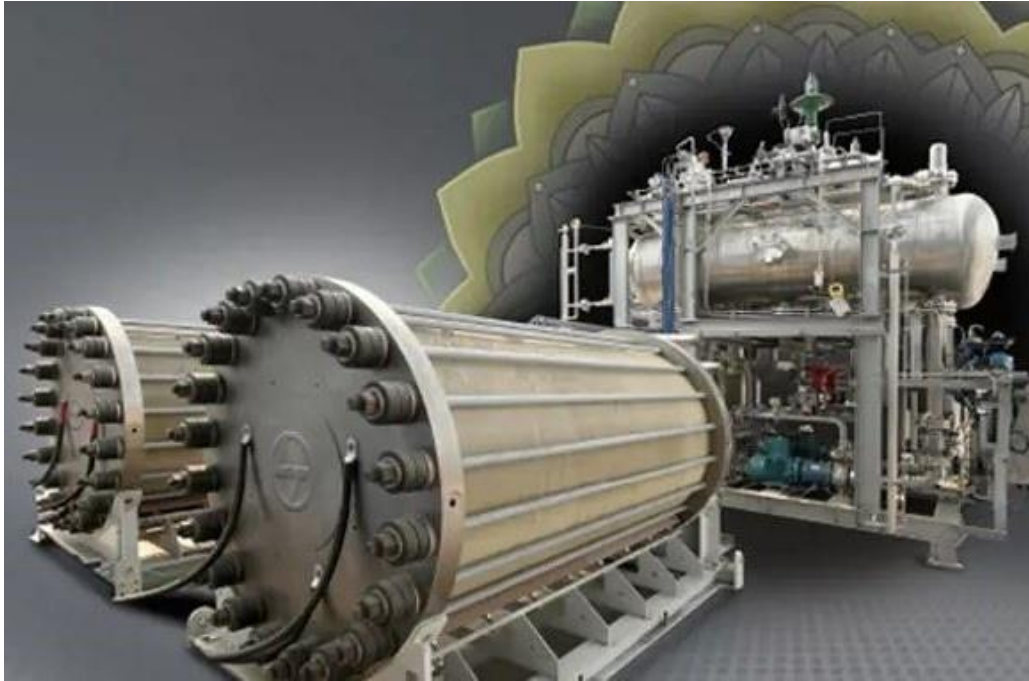


Andritz operating as EPC player to integrate Hydrogen Pro stacks into systems for projects in Europe, eg Salzgitter Flachstahl GmbH 100MW SALCOS® green steel project.





# Larsen & Toubro producing pressurised alkaline electrolyzers in India under license from McPhy.



# sbh4

## consulting

# Introduction to Stephen B. Harrison

**Stephen B. Harrison** is the founder and managing director at sbh4 GmbH in Germany. His work focuses on decarbonisation and greenhouse gas emissions reduction. E-fuels, hydrogen, ammonia and CCTUS are fundamental pillars of his consulting practice.

In support of the European Commission through CINEA in 2023, Stephen evaluated seven CCS, hydrogen and e-fuels submissions to the Third Innovation Fund. The fund allocated €2 billion to large-scale decarbonisation projects in Europe.

Stephen has served as the international expert and team leader for three ADB projects related to CCTUS and renewable hydrogen deployment in Pakistan, Palau and Viet Nam. He has also supported the IFC and work bank on e-fuels and green hydrogen strategy development projects in Namibia and Pakistan. In 2021, he specified more than 2GW of electrolyser capacity for green hydrogen projects.

With a background in industrial and specialty gases, including 27 years at BOC Gases, The BOC Group and Linde Gas, Stephen has intimate knowledge of e-fuels, hydrogen, ammonia and carbon dioxide from commercial, technical and operational perspectives. For 14 years, he was a global business leader in these FTSE100 and DAX30 companies.

Stephen has extensive buy-side and sell-side M&A due diligence and investment advisory experience in the energy and clean-tech sectors. Private Equity firms and investment fund managers and green-tech start-ups are regular clients. He also supports operating companies in their mission to decarbonise their scope 1, 2 and 3 GHG emissions.

Stephen served on the Scientific Committee for CEM2023 in Barcelona and chaired the session related to CEM from clean energy systems. Stephen was session chair for the e-fuels and hydrogen propulsion track at the Bremen Hydrogen Technology Exhibition in September 2023. He was also conference chair at the CO2 utilisation Summit in Hamburg in 2023. Stephen also served on the Technical Committee for the Green Hydrogen Summit in Oman in December 2022 and the Advisory Board of the International Power Summit in Munich in September 2022.

