## Pressure swing adsorption for CCS

Making the transition from oxygen production and hydrogen purification to clean energy

By Stephen B. Harrison, sbh4 consulting

he power generation and energy sectors will play a central role in the energy transition. Operating companies will pull for equipment and technology to build the infrastructure to capture, transport and sequestrate millions of tonnes of carbon dioxide (CO<sub>2</sub>) per year.

Industrial gases expertise and their engineering divisions will have a major supporting role to play in the quest for decarbonisation. Gas separation technologies that are well known within our industry, such as pressure swing adsorption (PSA) will have a central role to play.

Mature technologies to capture CO<sub>2</sub>
The components of a CCS scheme, from the absorption tower and stripper to the multi-stage CO<sub>2</sub> compressor with integrated drying system or CO<sub>2</sub> liquefier are mature.

Capturing CO<sub>2</sub> from SMR (steam methane reforming) process gases is well known to the urea fertiliser industry. Plant operators and equipment suppliers to the sector will have a depth of expertise to support

the energy transition. In this sector, the SMR is used to generate hydrogen for ammonia production. CO<sub>2</sub> is captured from the SMR and reacted with the ammonia to produce urea.

The standard carbon capture process in these applications uses an amine solvent. The flue gas is initially contacted with the solvent in an absorption column. CO, is captured by the amine solvent and removed from the flue gas before the residual gases are vented to atmosphere. The CO<sub>2</sub>-rich solvent is then pumped to a second stripping column where heat boils the CO, out of the solvent. The regenerated solvent is recirculated to the absorption tower to capture more CO<sub>2</sub>. The same CO<sub>2</sub> capture process can be used to decarbonise refinery SMR operations and enable existing assets to continue their operation with a vastly reduced CO<sub>2</sub> footprint.

PSA – a proven capture technology Moving beyond absorption processes for CO<sub>2</sub> capture, there are a host of alternative technologies that can be used to achieve the required gas separation. PSA, or its close relative vacuum swing adsorption (VSA) or a combined process of vacuum-pressure swing adsorption (VPSA) has been demonstrated to be effective for removing CO<sub>2</sub> from SMR process gases.

Air Products operates two SMRs at Port Arthur, Texas. The SMRs produce hydrogen which is supplied to the neighbouring Valero refinery. VSA technology has been implemented on both SMRs to capture CO<sub>2</sub> that is released during the process of converting natural gas feedstock to hydrogen. The resultant CO<sub>2</sub> is compressed, dried, and transferred to a nearby location through a pipeline. The CO<sub>2</sub> is utilised and permanently stored underground in an enhanced oil recovery scheme. This is an example of carbon capture, utilisation, and storage (CCUS).

SMRs generally use natural gas, refinery gas or naphtha as their feedstock. About 80% of global hydrogen production is derived from these fossil fuels using SMRs. The hydrocarbon feedstock is combined with steam and converted to syngas

over various reforming and water gas shift catalysts. The resultant syngas has a typical composition of 76% hydrogen, 17% CO<sub>2</sub>, and 7% unreacted methane and other gases. The syngas pressure is around 20 bar at this stage in the process.

An SMR typically emits 9.5kg of CO. per kg of hydrogen, making hydrogen produced by SMRs from fossil fuels without carbon capture unsustainable. To capture much of the CO, from the process gas on the Air Products SMRs, the VSA units have been inserted between the water gas shift reactors and the hydrogen purification PSA unit. This is a highly cost-effective location to capture the CO, due to the high pressure and high CO, concentration which combine to result in a high partial pressure of CO<sub>2</sub>. CO<sub>3</sub> can be produced from the VSA units with a purity of 95% and a recovery rate (from this process stream) of over 90%.

In addition to the process CO<sub>2</sub>, there are additional post combustion CO<sub>2</sub> emissions on the SMR which are more challenging to capture because the CO<sub>2</sub> concentration and the pressure are both low. However, the process and post combustion CO<sub>2</sub> emissions must be captured if a high overall CO<sub>2</sub> capture rate is required.

Adsorption-based gas separation The configuration and concept of a VSA system to capture  $CO_2$  is identical to the PSA systems that are used for other industrial gas separation applications such as purification of hydrogen from syngas that is produced by an SMR. PSA is used to generate medical oxygen from air in comparatively small systems. Similar systems are used to remove moisture from gas streams and are often referred to as regenerative dryers.

VPSA is used at larger scale to generate oxygen as an alternative to the cryogenic air separation

technology. Andreas Drescher,
Program Manager Carbon Reduction
at RHI MAGNESITA in Austria, says
that "we understand that VPSA is an
ideal choice for mid-range flow rates
where the required oxygen purity
is in the range of 90-95%. We have
therefore considered VPSA oxygen
generation as a cost-effective alternative
to liquid oxygen supplies for some
of our international raw material
production operations."

The operating principle behind the PSA, VSA and VPSA processes is the same. The gas mixture to be separated flows at an elevated pressure through a bed of small beads which are produced from a material that selectively adsorbs one of the gases in the mixture; the gases leaving the bed of beads no longer contain the gas that was selectively adsorbed.

These beads are referred to as a 'molecular sieve'. When they are loaded with the gas that they are sieving, the direction of the gas flow is reversed and the pressure in the adsorption bed is reduced. This swing in the pressure and flow direction releases the adsorbed gas. In a VSA or VPSA process, a vacuum pump is used to enhance this desorption process.

Drescher adds that, "There are a broad range of absorption, adsorption, biological and cryogenic processes for carbon capture and utilisation. Each can have merits based on the gas stream in question and the natural resources and infrastructure available in each location. Amongst a range of studies, we evaluated PSA for CO<sub>2</sub> capture from refractory material production on one of our plants."

Drescher is responsible for ensuring that RHI Magnesita will have the right technologies in place by 2025 to roll them out in its global operations subsequently. He says that "working on Project Green is an honour."

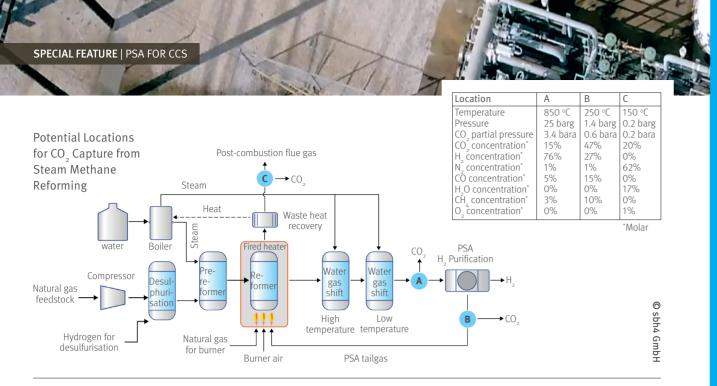
The company's long-term goal is to

"An SMR typically emits 9.5kg of CO<sub>2</sub> per kg of hydrogen, making hydrogen produced by SMRs from fossil fuels without carbon capture unsustainable..."

achieve climate neutral operations, but with the generation of geogenic CO<sub>2</sub> from calcination and post-combustion emissions to deal with too, this will be a major technological challenge and a range of new equipment will be required. "I studied geology, so getting to know more about gas separation processes and carbon capture has been a fascinating experience. In the Project Green team, we are keen to learn from operators in adjacent sectors and share our experience to accelerate the global path to decarbonisation."

CCS – from reservoirs to refineries
In the upstream oil and gas sector,
CO<sub>2</sub> released from sour gas processing
can be captured and stored to reduce
the carbon footprint of natural gas
extraction. CO<sub>2</sub> removal is essential
to enable natural gas liquefaction and
increase the calorific value of pipeline
natural gas. However, the captured CO<sub>2</sub>
is generally released to the atmosphere
at present. In the future, the captured
CO<sub>2</sub> will be transported as supercritical
gas or liquid CO<sub>2</sub> to a permanent
sequestration location, or will be
utilised in some way.

New facilities built to produce blue hydrogen must capture most of the CO<sub>2</sub> that is released from the reforming process chemistry and the post-combustion CO<sub>2</sub> emissions from the fired burners. The plant configuration for blue hydrogen production will most likely include an autothermal reformer



▶ (ATR) to convert the natural gas to syngas, which is then refined to yield the target hydrogen gas.

Despite the recent natural gas supply situation in Europe, several projects for blue hydrogen production from natural gas are in the pipeline in the UK and Norway. These countries have access to natural gas reserves in the North Sea and can use depleted oil and gas fields, or saline aquifers in the North Sea for underground CO<sub>2</sub> storage.

Established downstream refining operations can also reduce  $\mathrm{CO}_2$  emissions with CCS retrofits to existing process equipment. Capturing post-combustion  $\mathrm{CO}_2$  from steam boilers and fired heaters is possible.

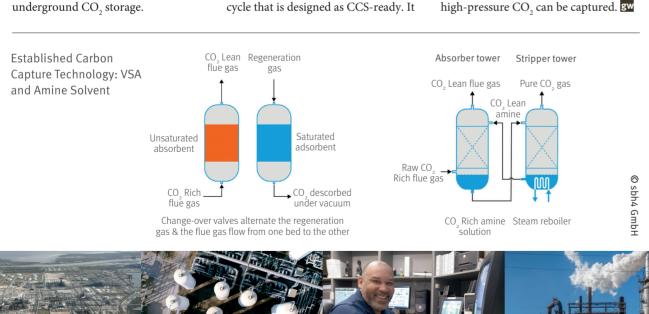
CO<sub>2</sub> emissions from thermal power generation fired with fossil fuels can also be reduced using CCS. New-build thermal power plants may wish to consider technologies such as the Allam cycle that is designed as CCS-ready. It

"...several projects for blue hydrogen production from natural gas are in the pipeline"

can be used with natural gas fired turbines or coal gasification. Oxyfuel combustion ensures a CO<sub>2</sub>-rich flue gas from which high-pressure CO<sub>2</sub> can be captured.

Refinery emissions, at Port Arthur

in Texas.



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Products' carbon capture unit.

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